

Card GAP test of Comp A-5

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English summary

Comp A-5 pressed to 95.4 %TMD (1.702 g/cm^3) has been tested in NOL Card Gap test. The transition between no go and go was found to be 222-3 cards or 56.5 mm. This result indicates that Comp A-5 is relatively shock sensitive compared to more modern PBX compositions.

Sammendrag

Comp A-5 presset til 95.4% av TMD (1.702 g/cm^3) er blitt testet i NOL Card GAP test.

Overgangen mellom ingen reaksjon og detonasjon ble funnet å være 222-3 kort eller 56.5 mm.

Dette resultatet tilsier at Comp A-5 har en relativ høy sjokkfølsomhet sammenlignet med mer moderne PBX komposisjoner.

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1 Introduction

STANAG 4488 (1) gives an overview of recommended tests for characterization of the shock sensitivity of energetic materials. For booster explosives there are two alternatives, a test using 20 mm and one using 40 mm charges. Normally we perform the 40 mm Intermediate Scale Gap test. However, since our object to be tested only can be filled into the test tubes by pressing we need a press tool. Since we at the moment do not have a pressing tool for charges with 40 mm diameter, but only a tool for 36 mm charges, we decided to use the NOL Card Gap test for testing the shock sensitivity of Comp A-5. This test uses the same barrier material in form of cellulose acetate cards as the intermediate scale gap test but a different booster material. The NOL Card Gap test uses two 80 g Tetryl Charges as booster (2).

2 Experimentally

2.1 The explosive

The tested explosive was produced by Dyno Nobel. Appendix A gives the control report of the tested explosive composition. Nammo Raufoss AS did perform the pressing of the pellets. Due to problems with releasing the pellets from the tool after pressing, some graphite had to be added.

2.2 Card GAP test

For testing the shock sensitivity of Comp A-5 we did use the standard NOL Card Gap test with two 80 g Tetryl pellets as boosters. The barrier was cellulose acetate cards with thickness 0.01

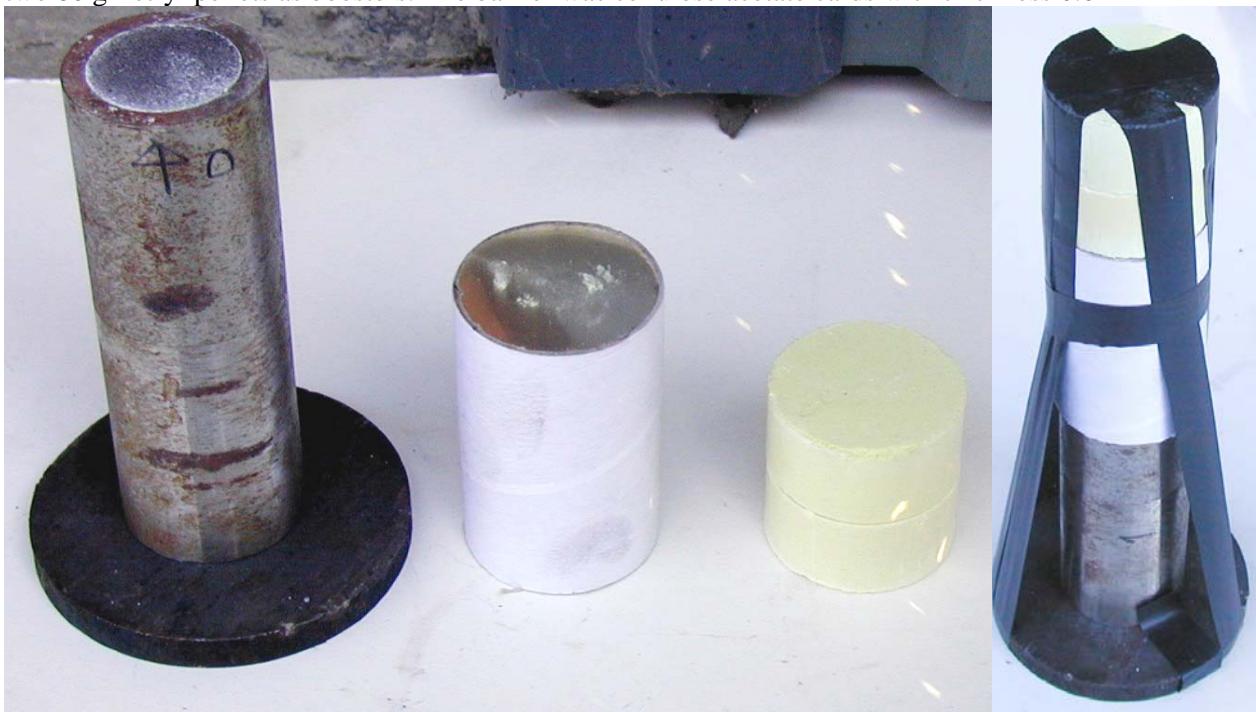


Figure 2.1 Pictures of shot No 1 before and after it was assembled.

inch or 2.54 mm. The test tubes were made from a seamless steel tube, length 140 mm, inner diameter 36.4 mm and wall thickness 6 mm. Figure 2.1 gives pictures of the tube, the cards and the boosters before and after assembling. To initiate the booster we used a detonator No. 8. The witness plate was a circular steel plate with diameter 110 mm.

2.3 Theoretical calculations

Theoretical calculations have been performed with Cheetah 2.0 code (3) for both TMD and the actual density we had for the pellets tested in NOL Card Gap test. Calculations have been performed with both the BKWC and the BKWS product databases. Complete printouts of these calculations are given in Appendix B.

3 Results

3.1 Density of tested Comp A-5 pellets

Table 3.1 gives the density of each tested pellet. To fill one tube we used 4 pellets which were glued together and to the steel tube. Figure 2.1 give a picture of tube No 1 after it was filled.

Tube No	Pellet No	Weight (g)	Diameter (mm)	Height (mm)	Volume (cm ³)	Density (g/cm ³)
1	1	60.34	36.03	34.68	35.359	1.707
	2	60.36	36.03	34.65	35.328	1.709
	3	60.35	36.03	34.63	35.308	1.709
	4	60.31	36.02	35.18	35.849	1.682
2	5	60.33	36.02	34.63	35.288	1.710
	6	60.34	36.02	34.58	35.237	1.712
	7	60.36	36.02	34.62	35.278	1.711
	8	60.36	36.02	34.62	35.278	1.711
3	9	60.37	36.02	34.68	35.339	1.708
	10	60.38	36.02	35.06	35.726	1.690
	11	60.38	36.03	34.64	35.318	1.710
	12	60.35	36.02	34.71	35.370	1.706
4	13	60.32	36.02	34.83	35.492	1.700
	14	60.37	36.01	34.96	35.605	1.696
	15	60.36	36.01	34.94	35.584	1.696
	16	60.33	36.01	34.97	35.615	1.694
7	17	60.32	36.02	34.70	35.360	1.706
	18	60.37	36.00	34.80	35.422	1.704
	19	60.36	36.01	35.08	35.727	1.689
	20	60.36	36.00	35.19	35.819	1.685
5	21	61.35	36.00	35.36	35.992	1.705
	22	61.00	35.99	35.41	36.023	1.693
	23	61.04	36.00	35.32	35.951	1.698
	24	61.04	36.00	35.23	35.860	1.702
6	25	60.37	36.00	34.96	35.585	1.697
	26	61.33	36.00	35.34	35.972	1.705
	27	61.22	35.99	35.68	36.298	1.687
	28	60.81	35.99	35.33	35.942	1.692
8	29	59.82	36.01	34.33	34.963	1.711
	30	61.33	35.99	35.41	36.023	1.703
	31	61.37	36.00	35.31	35.941	1.708
	32	61.27	35.99	35.22	35.830	1.710
9	33	61.33	35.99	35.19	35.799	1.713
	34	61.35	36.00	35.23	35.860	1.711
	35	61.38	36.01	35.11	35.757	1.717
	36	61.36	36.00	35.07	35.697	1.719
10	37	60.34	36.00	35.06	35.687	1.691
	38	61.29	36.00	35.18	35.809	1.712
	39	60.25	36.01	34.63	35.269	1.708
	40	60.82	36.00	35.70	36.338	1.674
		Average				1.702+0.010

Table 3.1 Density of Comp A-5 pellets used in Card GAP Test.

Obtained density of the Comp A-5 pellets was 1.702 g/cm^3 . TMD for this charge of Comp A-5 is 1.7847 g/cm^3 . The obtained pellet density is therefore only 95.37 % of TMD.

3.2 Card Gap Test

Ten tubes were filled and tested in the NOL Card Gap test. For the first shot we started with a barrier thickness of 200 cards or 51 mm. The first shot went to full detonation as the picture of the witness plate in Figure 3.1 shows. For the second shot we increased the barrier thickness to 230 cards. This time we obtained no reaction as the picture of the witness plate in Figure 3.2 shows. The witness plate is intact without any hole and only a moderate dent. After getting conformation of that a barrier of 230 cards was a safe distance by firing additional two shots with a barrier thickness of 230 cards, we reduced the barrier thickness for the following shots. First we reduced the barrier thickness to 220 cards than to 225 cards before the last shot was fired with a barrier thickness of 220 cards. In Figures 3.3 to 3.10 are pictures of all witness plates in addition to other rests from each of these 8 shots given.



Figure 3.1 Shot No 1, tube No 1, barrier thickness 200 cards, detonation.



Figure 3.2 Shot No 2, tube No 2, barrier thickness 230 cards, no reaction.



Figure 3.3 Shot No 3, tube No 3, barrier 230 cards, no reaction.



Figure 3.4 Shot No 4, tube No 4, barrier 230 cards, no reaction.



Figure 3.5 Shot No 5, tube No 5, barrier 220 cards, detonation.



Figure 3.6 Shot No 6, tube No 6, barrier 220 cards, detonation.



Figure 3.7 Shot No 7, tube No 7, barrier 225 cards, no reaction.



Figure 3.8 Shot No 8, tube No 8, barrier 225 cards, no reaction.



Figure 3.9 Shot No 9, tube No 9, barrier 225 cards, no reaction.



Figure 3.10 Shot No 10, tube No10, barrier 220 cards, detonation.

Shot No.	Tube No.	Barrier Thickness (Cards)	Barrier Thickness (mm)	Reaction
1	1	200	50.8	Detonation
2	2	230	58.2	No Reaction
3	3	230	58.2	No Reaction
4	4	230	58.2	No Reaction
5	5	220	55.88	Detonation
6	6	220	55.88	Detonation
7	7	225	57.15	No Reaction
8	8	225	57.15	No Reaction
9	9	225	57.15	No Reaction
10	10	220	55.88	Detonation

Table 3.2 Summary of the results of the firings in Card GAP-test of Comp A-5.

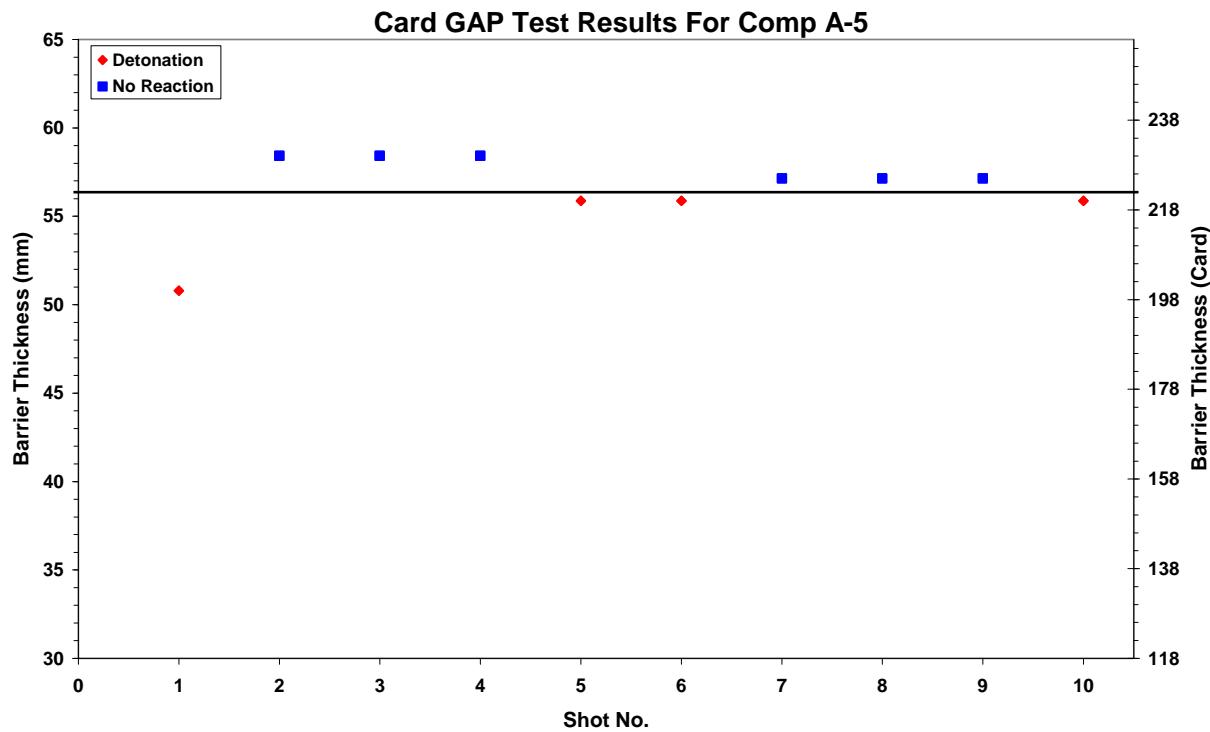


Figure 3.11 Plot of the results in Card Gap test for Comp A-5.

Table 3.2 summarizes the results for all ten tested tubes. Figure 3.11 gives a plot of the Comp A-5 test series. From Table 3.2 and Figure 3.11 we can see that the transition between full detonation and no reaction is narrow. All shots with barrier thickness of 225 cards or more gave no reaction while shots with barrier thickness of 220 cards or lower went all to full detonation. The obtained result of 222.3 cards or 56.5 mm in barrier thickness for the transition between a no go/go reactions indicates that Comp A-5 is a relative shock sensitive composition.

3.3 Theoretical calculations

Performance of Comp A-5 at TMD (Theoretical Maximum Density) is higher with respect to both detonation velocity and pressure compared with Octol 70/30 (HMX/TNT). However compared with press filled HMX/Binder (95/5) compositions as for example PBXN-5 has Comp A-5 approximately 10% lower detonation pressure and 200 m/s lower detonation velocity. For fillings of Comp A-5 with density equal to those tested in the NOL Card Gap test, the actually product density will give a reduction in detonation pressure of 10% and in the velocity of 300 m/s, Table 3.3, compares with a filling of TMD.

Properties at C-J condition	Comp A-5				PBXN-5*	Octol 70/30
Density g/cm³	1.78467		1.7020		1.9031	1.8220
Product library	BKWC	BKWS	BKWC	BKWS	BKWC	BKWC
Pressure (GPa)	33.27	32.88	29.74	29.57	36.64	32.29
Volume (cc/g)	0.425	0.430	0.444	0.448	0.400	0.413
Density (g/cc)	2.355	2.327	2.250	2.233	2.502	2.421
Energy (kJ/cc)	4.03	3.83	3.62	3.52	4.39	3.99
Temperature (K)	4148	4085	4191	4140	3987	4033
Shock velocity (m/s)	8776	8891	8471	8549	8966	8463
Particle velocity (m/s)	2125	2072	2063	2032	2147	2094
Speed of sound (m/s)	6651	6818	6408	6517	6819	6370
Gamma	3.131	3.290	3.107	3.206	3.176	3.042
Freezing at 1800 K gives						
Total energy of detonation (kJ/cc)	-10.179	-10.444	-9.554	-9.825	-10.702	-9.949

*HMX/Viton (95/5) + 0.5wt.% Graphite added.

Table 3.3 Cheetah 2.0 Code calculated properties for Comp A-5, PBXN-5 and Octol 70/30.

Appendix A

A.1 Control report for tested composition

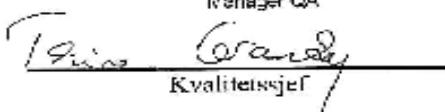
DYNO High Energy Materials		KONTROLLRAPPORT: i henhold til EN 10204 - 3.1				
Kjoper/Mottaker Nammo Raufoss AS Postboks 162 2831 Raufoss		Bestillingsnummer 58159-0/ROEST/3 Bestillingsdato 16.02.07	Rapport nummer 088 Kontroll dato 22.02.07			
Produsent Dyno Nobel ASA N-3176 Sætre NORGE		Produksjonsdato 13.11.06	Offentlig oppdragssummer			
Løs nummer DDP07B0056-0001		Mengde 20 kg	Art.nr. 0166819			
Sprengstofftype Composition A-5, Klasse 2		Leveringsbetingelser/ Teknisk underlag MIL-DTL-14970D				
Analyseresultater						
	Sammenstilling		Tuktighet	Volumvekt	Ulike partikler på	
	RDX	Stearinsyre			USSS nr. 40	USSS nr. 60
Spesifikasjon	98,5 - 99,0 %	1,0 - 1,5 %	$\leq 0,10\%$	$\geq 0,95 \text{ g/ml}$	0	Max. 5
Charge nr. 03/06	98,7	1,3	0,02	1,07	0	0
	Konsentrering, % gjennom USSS nr.		Gap Test		Cylklobeksand, %	
	12	200	Regular detonation	Regular not detonation		
Spesifikasjon	> 99,0	$\leq 2,4$	mm H ₂ O	$\leq 28 \text{ mm H}_2\text{O}$	$\leq 0,30$	
Charge nr. 03/06	100	0,7	-	-	0,19	
DYNO High Energy Materials Manager QA 						

Figure A.1 Control report for Comp A-5 class 2.

Appendix B Complete printout for standard Cheetah run

B.1 Product library BKWS

Product library title: bkws library
 Executing library command: gas eos, bkw
 Executing library command: set, bkw, alpha, 0.5
 Executing library command: set, bkw, beta, 0.298
 Executing library command: set, bkw, theta, 6620.
 Executing library command: set, bkw, kappa, 10.5
 Input>composition, steacid, 1.3, rdx, 98.7, weight

Name	The Composition			Heat of formation (cal/mol)	Standard volume (cc/mol)	Standard entropy (cal/K/mol)	Mol. wt.	Formula
	% wt.	% mol	% vol.					
RDX	98.70	98.98	97.53	16496	122.99	0.000	222.13	C ₃ H ₆ N ₆ O ₆
Stearacid	1.30	1.02	2.47	-228967	302.30	0.000	284.47	C ₁₈ H ₃₆ O ₂

Heat of formation = 62.836 cal/gm
 Standard volume = 0.560 cc/gm
 Standard entropy = 0.000 cal/k/gm
 Standard energy = 62.822 cal/gm

The elements and percent by mole
 c 14.762
 h 29.525
 o 27.904
 n 27.809

The average mol. wt. = 222.761 g/mol

Input>gas eos, bkw

Input>standard run, rho, 1.784673

The hugoniot reference state:

P0 = 1.000000 ATM, V0 = 0.560327 cc/gm, E0 = 62.822270 cal/gm

Using 149504 ATM as a lower bound for the C-J pressure

Using 373760 ATM as an upper bound for the C-J pressure

The C-J point was bracketed in cjbrent

The CJ state was found in 6 iterations

The C-J condition

The shock velocity = 8.89067e+003 m/s
 The particle velocity = 2.07219e+003 m/s
 The speed of sound = 6.81848e+003 m/s

P0 = 1 atm, V0 = 0.56033 cc/gm, E0 = 62.82227 cal/gm

Reference state = reactants
 H(R) = H-62.84, E(R) = E-62.82, S(R) = S- 0.00

P (ATM)	V (CC/GM)	T (K)	H(R) (CAL/GM)	E(R) (CAL/GM)	S(R) (CAL/K/GM)	VGS (CC/GM)
1.) 324494.5	0.4297	4084.9	3890.22	513.16	1.676	0.4288

Product concentrations

Name	(mol/kg)	(mol gas/mol explosive)
n2 Gas	1.255e+001	2.795e+000
co2 Gas	8.742e+000	1.947e+000
h2o Gas	4.604e+000	1.026e+000
ch2o2 Gas	2.178e+000	4.851e-001
h3n Gas	1.467e+000	3.269e-001
c2h6 Gas	9.434e-001	2.102e-001
ch4 Gas	8.112e-001	1.807e-001
h2 Gas	2.094e-001	4.665e-002
ch3oh Gas	1.943e-001	4.329e-002
co Gas	5.659e-002	1.261e-002
h4n2 Gas	3.181e-002	7.086e-003
no Gas	2.441e-002	5.439e-003

c2h4	Gas	1.109e-002	2.471e-003
ch3	Gas	8.717e-003	1.942e-003
h2o2	Gas	7.503e-003	1.671e-003
o2	Gas	4.584e-003	1.021e-003
h2n	Gas	4.402e-003	9.805e-004
ch2o	Gas	3.417e-003	7.611e-004
h2n2	Gas	2.420e-003	5.391e-004
ho	Gas	2.059e-003	4.587e-004
cno	Gas	1.585e-003	3.530e-004
chno	Gas	1.152e-003	2.566e-004
h	Gas	9.913e-004	2.208e-004
o	Gas	3.824e-004	8.519e-005
no2	Gas	1.767e-004	3.936e-005
c3h8	Gas	7.961e-005	1.773e-005
ch2	Gas	7.525e-005	1.676e-005
ho2	Gas	5.443e-005	1.213e-005
cho	Gas	4.639e-005	1.033e-005
hno	Gas	4.169e-005	9.288e-006
chn	Gas	2.971e-005	6.618e-006
n	Gas	2.374e-005	5.288e-006
n2o	Gas	2.312e-005	5.151e-006
hn	Gas	1.031e-005	2.297e-006
c2h2	Gas	7.572e-006	1.687e-006
cn	Gas	4.199e-006	9.353e-007
n3	Gas	1.664e-006	3.707e-007
no3	Gas	1.586e-006	3.533e-007
hno2	Gas	9.297e-007	2.071e-007
c3h6	Gas	8.751e-007	1.949e-007
cn2	Gas	7.782e-007	1.733e-007
hno3	Gas	7.792e-008	1.736e-008
ch	Gas	7.435e-008	1.656e-008
c2h	Gas	3.605e-008	8.031e-009
no2h	Gas	2.313e-008	5.153e-009
c	Gas	1.663e-008	3.705e-009
o3	Gas	4.950e-009	1.103e-009
n2o4	Gas	4.033e-009	8.984e-010
c2n2	Gas	1.215e-009	2.707e-010
c2h4o	Gas	6.213e-010	1.384e-010
c2n	Gas	4.678e-010	1.042e-010
c2	Gas	4.514e-010	1.006e-010
c2o	Gas	9.663e-011	2.153e-011
n2o3	Gas	2.853e-011	6.356e-012
cnn	Gas	1.503e-011	3.347e-012
c3o2	Gas	2.898e-013	6.456e-014
c3	Gas	7.832e-014	1.745e-014
n2o5	Gas	4.496e-014	1.001e-014
c4	Gas	2.919e-023	6.501e-024
c4n2	Gas	1.562e-031	3.479e-032
c5	Gas	3.842e-034	8.557e-035
*c	solid	2.471e-001	5.503e-002
*h2o	liquid	0.000e+000	0.000e+000
Total	Gas	3.186e+001	7.097e+000
Total	Cond.	2.471e-001	5.503e-002

The C-J Adiabat

Reference state = reactants
 $H(R) = H-62.84$, $E(R) = E-62.82$, $S(R) = S- 0.00$

P (ATM)	V (CC/GM)	T (K)	H(R) (CAL/GM)	E(R) (CAL/GM)	S(R) (CAL/K/GM)	VGS (CC/GM)
1.) 139677.1	0.5603	3290.5	1730.88	-164.53	1.676	0.5512

Product concentrations

Name	(mol/kg)	(mol gas/mol explosive)
n2 Gas	1.276e+001	2.842e+000
co2 Gas	8.786e+000	1.957e+000
h2o Gas	7.159e+000	1.595e+000

ch4	Gas	1.289e+000	2.872e-001
h3n	Gas	1.130e+000	2.517e-001
h2	Gas	8.504e-001	1.894e-001
ch2o2	Gas	7.018e-001	1.563e-001
co	Gas	5.138e-001	1.145e-001
c2h6	Gas	3.091e-001	6.885e-002
ch3oh	Gas	8.411e-002	1.874e-002
c2h4	Gas	1.823e-002	4.062e-003
ch3	Gas	1.090e-002	2.429e-003
ch2o	Gas	1.047e-002	2.333e-003
chno	Gas	3.625e-003	8.074e-004
no	Gas	2.802e-003	6.241e-004
h2n	Gas	2.062e-003	4.593e-004
h	Gas	1.417e-003	3.156e-004
ho	Gas	1.401e-003	3.120e-004
h4n2	Gas	1.301e-003	2.899e-004
chn	Gas	5.667e-004	1.262e-004
h2o2	Gas	2.693e-004	6.000e-005
cho	Gas	2.345e-004	5.223e-005
cno	Gas	1.939e-004	4.320e-005
h2n2	Gas	1.878e-004	4.184e-005
c3h8	Gas	1.470e-004	3.274e-005
o2	Gas	9.995e-005	2.226e-005
c2h2	Gas	8.359e-005	1.862e-005
ch2	Gas	3.388e-005	7.547e-006
o	Gas	2.389e-005	5.321e-006
c3h6	Gas	1.277e-005	2.845e-006
hno	Gas	1.183e-005	2.634e-006
hn	Gas	4.224e-006	9.409e-007
n2o	Gas	3.918e-006	8.728e-007
cn	Gas	3.700e-006	8.243e-007
ho2	Gas	2.991e-006	6.664e-007
n	Gas	2.114e-006	4.709e-007
no2	Gas	2.056e-006	4.580e-007
cn2	Gas	1.763e-007	3.928e-008
c2h	Gas	1.607e-007	3.581e-008
hno2	Gas	1.564e-007	3.483e-008
n3	Gas	1.202e-007	2.679e-008
c2n2	Gas	3.774e-008	8.407e-009
ch	Gas	2.738e-008	6.099e-009
no2h	Gas	1.368e-008	3.048e-009
c2h4o	Gas	9.142e-009	2.037e-009
c2n	Gas	2.519e-009	5.611e-010
c2o	Gas	2.287e-009	5.094e-010
c	Gas	2.012e-009	4.482e-010
hno3	Gas	4.048e-010	9.018e-011
c3o2	Gas	2.369e-010	5.276e-011
no3	Gas	2.356e-010	5.248e-011
c2	Gas	6.859e-011	1.528e-011
cnn	Gas	2.082e-011	4.639e-012
o3	Gas	9.400e-012	2.094e-012
c3	Gas	3.890e-013	8.665e-014
n2o3	Gas	1.091e-013	2.431e-014
n2o4	Gas	2.726e-014	6.073e-015
n2o5	Gas	2.331e-019	5.192e-020
c4	Gas	8.594e-021	1.914e-021
c4n2	Gas	4.638e-024	1.033e-024
c5	Gas	3.717e-028	8.281e-029
*c	solid	2.097e+000	4.671e-001
*h2o	liquid	0.000e+000	0.000e+000
Total	Gas	3.364e+001	7.493e+000
Total	Cond.	2.097e+000	4.671e-001

Reference state = reactants
 $H(R) = H-62.84$, $E(R) = E-62.82$, $S(R) = S- 0.00$

P (ATM)	V (CC/GM)	T (K)	H(R) (CAL/GM)	E(R) (CAL/GM)	S(R) (CAL/K/GM)	VGS (CC/GM)
------------	--------------	----------	------------------	------------------	--------------------	----------------

1.) 15005.7 1.2307 1800.0 -481.68 -928.91 1.676 1.2235

Product concentrations

	Name	(mol/kg)	(mol gas/mol explosive)
	n2 Gas	1.318e+001	2.937e+000
	h2o Gas	8.023e+000	1.787e+000
	co2 Gas	7.781e+000	1.733e+000
	co Gas	3.126e+000	6.963e-001
	h2 Gas	2.150e+000	4.789e-001
	ch4 Gas	1.729e+000	3.850e-001
	h3n Gas	2.901e-001	6.462e-002
	c2h6 Gas	1.835e-002	4.088e-003
	ch2o2 Gas	1.735e-002	3.865e-003
	ch2o Gas	3.414e-003	7.605e-004
	c2h4 Gas	2.713e-003	6.044e-004
	ch3oh Gas	2.294e-003	5.110e-004
	chn Gas	1.872e-003	4.171e-004
	chno Gas	1.277e-003	2.845e-004
	ch3 Gas	2.276e-004	5.071e-005
	c3h8 Gas	3.856e-005	8.590e-006
	c3h6 Gas	2.064e-005	4.598e-006
	c2h2 Gas	1.924e-005	4.286e-006
	h Gas	1.869e-005	4.163e-006
	cho Gas	1.205e-005	2.685e-006
	h2n Gas	4.527e-006	1.008e-006
	ho Gas	3.073e-006	6.846e-007
	no Gas	2.976e-007	6.630e-008
	h4n2 Gas	8.554e-008	1.905e-008
	h2n2 Gas	1.503e-008	3.349e-009
	c2n2 Gas	1.418e-008	3.160e-009
	cno Gas	7.903e-009	1.760e-009
	c3o2 Gas	7.845e-009	1.747e-009
	ch2 Gas	2.639e-009	5.879e-010
	c2h4o Gas	1.957e-009	4.359e-010
	h2o2 Gas	1.673e-009	3.726e-010
	hno Gas	1.621e-009	3.612e-010
	cn Gas	9.501e-010	2.117e-010
	n2o Gas	5.291e-010	1.179e-010
	hn Gas	3.304e-010	7.360e-011
	c2h Gas	1.520e-010	3.385e-011
	o2 Gas	9.402e-011	2.094e-011
	o Gas	5.298e-011	1.180e-011
	c2o Gas	1.894e-011	4.219e-012
	n Gas	5.752e-012	1.281e-012
	ho2 Gas	4.443e-012	9.898e-013
	hno2 Gas	3.294e-012	7.338e-013
	cn2 Gas	1.849e-012	4.119e-013
	no2h Gas	1.647e-012	3.669e-013
	c2n Gas	7.691e-013	1.713e-013
	n3 Gas	3.898e-013	8.684e-014
	no2 Gas	2.912e-013	6.487e-014
	ch Gas	4.700e-014	1.047e-014
	cnn Gas	2.758e-016	6.143e-017
	c Gas	1.288e-016	2.869e-017
	c4n2 Gas	4.458e-018	9.931e-019
	hno3 Gas	2.100e-018	4.678e-019
	c3 Gas	1.701e-018	3.788e-019
	c2 Gas	8.361e-019	1.863e-019
	no3 Gas	3.135e-022	6.983e-023
	o3 Gas	1.438e-022	3.203e-023
	n2o3 Gas	6.317e-024	1.407e-024
	c4 Gas	4.561e-025	1.016e-025
	c5 Gas	1.419e-027	3.161e-028
	n2o4 Gas	9.859e-030	2.196e-030
	n2o5 Gas	4.367e-037	9.729e-038
	*c solid	1.449e+000	3.228e-001
	*h2o liquid	0.000e+000	0.000e+000
	Total Gas	3.633e+001	8.093e+000

Total Cond. 1.449e+000 3.228e-001

Reference state = reactants
 $H(R) = H-62.84$, $E(R) = E-62.82$, $S(R) = S- 0.00$

	P (ATM)	V (CC/GM)	T (K)	$H(R)$ (CAL/GM)	$E(R)$ (CAL/GM)	$S(R)$ (CAL/K/GM)	VGS (CC/GM)
1.)	14942.0	1.2327	1798.2	-483.58	-929.65	1.676	1.2255

Product concentrations

	Name	(mol/kg)	(mol gas/mol explosive)
*	n2	Gas 1.318e+001	2.937e+000
*	h2o	Gas 8.023e+000	1.787e+000
*	co2	Gas 7.781e+000	1.733e+000
*	co	Gas 3.126e+000	6.963e-001
*	h2	Gas 2.150e+000	4.789e-001
*	ch4	Gas 1.729e+000	3.850e-001
*	h3n	Gas 2.901e-001	6.462e-002
*	c2h6	Gas 1.835e-002	4.088e-003
*	ch2o2	Gas 1.735e-002	3.865e-003
*	ch2o	Gas 3.414e-003	7.605e-004
*	c2h4	Gas 2.713e-003	6.044e-004
*	ch3oh	Gas 2.294e-003	5.110e-004
*	chn	Gas 1.872e-003	4.171e-004
*	chno	Gas 1.277e-003	2.845e-004
*	ch3	Gas 2.276e-004	5.071e-005
*	c3h8	Gas 3.856e-005	8.590e-006
*	c3h6	Gas 2.064e-005	4.598e-006
*	c2h2	Gas 1.924e-005	4.286e-006
*	h	Gas 1.869e-005	4.163e-006
*	cho	Gas 1.205e-005	2.685e-006
*	h2n	Gas 4.527e-006	1.008e-006
*	ho	Gas 3.073e-006	6.846e-007
*	no	Gas 2.976e-007	6.630e-008
*	h4n2	Gas 8.554e-008	1.905e-008
*	h2n2	Gas 1.503e-008	3.349e-009
*	c2n2	Gas 1.418e-008	3.160e-009
*	cno	Gas 7.903e-009	1.760e-009
*	c3o2	Gas 7.845e-009	1.747e-009
*	ch2	Gas 2.639e-009	5.879e-010
*	c2h4o	Gas 1.957e-009	4.359e-010
*	h2o2	Gas 1.673e-009	3.726e-010
*	hno	Gas 1.621e-009	3.612e-010
*	cn	Gas 9.501e-010	2.117e-010
*	n2o	Gas 5.291e-010	1.179e-010
*	hn	Gas 3.304e-010	7.360e-011
*	c2h	Gas 1.520e-010	3.385e-011
*	o2	Gas 9.402e-011	2.094e-011
*	o	Gas 5.298e-011	1.180e-011
*	c2o	Gas 1.894e-011	4.219e-012
*	n	Gas 5.752e-012	1.281e-012
*	ho2	Gas 4.443e-012	9.898e-013
*	hno2	Gas 3.294e-012	7.338e-013
*	cn2	Gas 1.849e-012	4.119e-013
*	no2h	Gas 1.647e-012	3.669e-013
*	c2n	Gas 7.691e-013	1.713e-013
*	n3	Gas 3.898e-013	8.684e-014
*	no2	Gas 2.912e-013	6.487e-014
*	ch	Gas 4.700e-014	1.047e-014
*	cnn	Gas 2.758e-016	6.143e-017
*	c	Gas 1.288e-016	2.869e-017
*	c4n2	Gas 4.458e-018	9.931e-019
*	hno3	Gas 2.100e-018	4.678e-019
*	c3	Gas 1.701e-018	3.788e-019
*	c2	Gas 8.361e-019	1.863e-019
*	no3	Gas 3.135e-022	6.983e-023
*	o3	Gas 1.438e-022	3.203e-023
*	n2o3	Gas 6.317e-024	1.407e-024
*	c4	Gas 4.561e-025	1.016e-025

*	c5	Gas	1.419e-027	3.161e-028
*	n2o4	Gas	9.859e-030	2.196e-030
*	n2o5	Gas	4.367e-037	9.729e-038
*	*c	solid	1.449e+000	3.228e-001
*	*h2o	liquid	0.000e+000	0.000e+000

Total	Gas	3.633e+001	8.093e+000
Total	Cond.	1.449e+000	3.228e-001

Reference state = reactants
 $H(R) = H-62.84$, $E(R) = E-62.82$, $S(R) = S- 0.00$

	P (ATM)	V (CC/GM)	T (K)	H(R) (CAL/GM)	E(R) (CAL/GM)	S(R) (CAL/K/GM)	VGS (CC/GM)
1.)	3566.9	2.2973	1314.1	-916.69	-1115.13	1.676	2.2901

Product concentrations

	Name	(mol/kg)	(mol gas/mol explosive)
*	n2	Gas 1.318e+001	2.937e+000
*	h2o	Gas 8.023e+000	1.787e+000
*	co2	Gas 7.781e+000	1.733e+000
*	co	Gas 3.126e+000	6.963e-001
*	h2	Gas 2.150e+000	4.789e-001
*	ch4	Gas 1.729e+000	3.850e-001
*	h3n	Gas 2.901e-001	6.462e-002
*	c2h6	Gas 1.835e-002	4.088e-003
*	ch2o2	Gas 1.735e-002	3.865e-003
*	ch2o	Gas 3.414e-003	7.605e-004
*	c2h4	Gas 2.713e-003	6.044e-004
*	ch3oh	Gas 2.294e-003	5.110e-004
*	chn	Gas 1.872e-003	4.171e-004
*	chno	Gas 1.277e-003	2.845e-004
*	ch3	Gas 2.276e-004	5.071e-005
*	c3h8	Gas 3.856e-005	8.590e-006
*	c3h6	Gas 2.064e-005	4.598e-006
*	c2h2	Gas 1.924e-005	4.286e-006
*	h	Gas 1.869e-005	4.163e-006
*	cho	Gas 1.205e-005	2.685e-006
*	h2n	Gas 4.527e-006	1.008e-006
*	ho	Gas 3.073e-006	6.846e-007
*	no	Gas 2.976e-007	6.630e-008
*	h4n2	Gas 8.554e-008	1.905e-008
*	h2n2	Gas 1.503e-008	3.349e-009
*	c2n2	Gas 1.418e-008	3.160e-009
*	cno	Gas 7.903e-009	1.760e-009
*	c3o2	Gas 7.845e-009	1.747e-009
*	ch2	Gas 2.639e-009	5.879e-010
*	c2h4o	Gas 1.957e-009	4.359e-010
*	h2o2	Gas 1.673e-009	3.726e-010
*	hno	Gas 1.621e-009	3.612e-010
*	cn	Gas 9.501e-010	2.117e-010
*	n2o	Gas 5.291e-010	1.179e-010
*	hn	Gas 3.304e-010	7.360e-011
*	c2h	Gas 1.520e-010	3.385e-011
*	o2	Gas 9.402e-011	2.094e-011
*	o	Gas 5.298e-011	1.180e-011
*	c2o	Gas 1.894e-011	4.219e-012
*	n	Gas 5.752e-012	1.281e-012
*	ho2	Gas 4.443e-012	9.898e-013
*	hno2	Gas 3.294e-012	7.338e-013
*	cn2	Gas 1.849e-012	4.119e-013
*	no2h	Gas 1.647e-012	3.669e-013
*	c2n	Gas 7.691e-013	1.713e-013
*	n3	Gas 3.898e-013	8.684e-014
*	no2	Gas 2.912e-013	6.487e-014
*	ch	Gas 4.700e-014	1.047e-014
*	cnn	Gas 2.758e-016	6.143e-017
*	c	Gas 1.288e-016	2.869e-017
*	c4n2	Gas 4.458e-018	9.931e-019

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*   hno3  Gas  2.100e-018  4.678e-019
*   c3    Gas  1.701e-018  3.788e-019
*   c2    Gas  8.361e-019  1.863e-019
*   no3   Gas  3.135e-022  6.983e-023
*   o3    Gas  1.438e-022  3.203e-023
*   n2o3  Gas  6.317e-024  1.407e-024
*   c4    Gas  4.561e-025  1.016e-025
*   c5    Gas  1.419e-027  3.161e-028
*   n2o4  Gas  9.859e-030  2.196e-030
*   n2o5  Gas  4.367e-037  9.729e-038
*   *c    solid 1.449e+000  3.228e-001
*   *h2o   liquid 0.000e+000  0.000e+000

Total Gas  3.633e+001  8.093e+000
Total Cond. 1.449e+000  3.228e-001

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Reference state = reactants
 $H(R) = H-62.84$, $E(R) = E-62.82$, $S(R) = S- 0.00$

	P (ATM)	V (CC/GM)	T (K)	H(R) (CAL/GM)	E(R) (CAL/GM)	S(R) (CAL/K/GM)	VGS (CC/GM)
1.)	1464.1	3.6421	1093.1	-1059.62	-1188.75	1.676	3.6348

Product concentrations

	Name	(mol/kg)	(mol gas/mol explosive)
*	n2	Gas 1.318e+001	2.937e+000
*	h2o	Gas 8.023e+000	1.787e+000
*	co2	Gas 7.781e+000	1.733e+000
*	co	Gas 3.126e+000	6.963e-001
*	h2	Gas 2.150e+000	4.789e-001
*	ch4	Gas 1.729e+000	3.850e-001
*	h3n	Gas 2.901e-001	6.462e-002
*	c2h6	Gas 1.835e-002	4.088e-003
*	ch2o2	Gas 1.735e-002	3.865e-003
*	ch2o	Gas 3.414e-003	7.605e-004
*	c2h4	Gas 2.713e-003	6.044e-004
*	ch3oh	Gas 2.294e-003	5.110e-004
*	chn	Gas 1.872e-003	4.171e-004
*	chno	Gas 1.277e-003	2.845e-004
*	ch3	Gas 2.276e-004	5.071e-005
*	c3h8	Gas 3.856e-005	8.590e-006
*	c3h6	Gas 2.064e-005	4.598e-006
*	c2h2	Gas 1.924e-005	4.286e-006
*	h	Gas 1.869e-005	4.163e-006
*	cho	Gas 1.205e-005	2.685e-006
*	h2n	Gas 4.527e-006	1.008e-006
*	ho	Gas 3.073e-006	6.846e-007
*	no	Gas 2.976e-007	6.630e-008
*	h4n2	Gas 8.554e-008	1.905e-008
*	h2n2	Gas 1.503e-008	3.349e-009
*	c2n2	Gas 1.418e-008	3.160e-009
*	cno	Gas 7.903e-009	1.760e-009
*	c3o2	Gas 7.845e-009	1.747e-009
*	ch2	Gas 2.639e-009	5.879e-010
*	c2h4o	Gas 1.957e-009	4.359e-010
*	h2o2	Gas 1.673e-009	3.726e-010
*	hno	Gas 1.621e-009	3.612e-010
*	cn	Gas 9.501e-010	2.117e-010
*	n2o	Gas 5.291e-010	1.179e-010
*	hn	Gas 3.304e-010	7.360e-011
*	c2h	Gas 1.520e-010	3.385e-011
*	o2	Gas 9.402e-011	2.094e-011
*	o	Gas 5.298e-011	1.180e-011
*	c2o	Gas 1.894e-011	4.219e-012
*	n	Gas 5.752e-012	1.281e-012
*	ho2	Gas 4.443e-012	9.898e-013
*	hno2	Gas 3.294e-012	7.338e-013
*	cn2	Gas 1.849e-012	4.119e-013
*	no2h	Gas 1.647e-012	3.669e-013

*	c2n	Gas	7.691e-013	1.713e-013
*	n3	Gas	3.898e-013	8.684e-014
*	no2	Gas	2.912e-013	6.487e-014
*	ch	Gas	4.700e-014	1.047e-014
*	cnn	Gas	2.758e-016	6.143e-017
*	c	Gas	1.288e-016	2.869e-017
*	c4n2	Gas	4.458e-018	9.931e-019
*	hno3	Gas	2.100e-018	4.678e-019
*	c3	Gas	1.701e-018	3.788e-019
*	c2	Gas	8.361e-019	1.863e-019
*	no3	Gas	3.135e-022	6.983e-023
*	o3	Gas	1.438e-022	3.203e-023
*	n2o3	Gas	6.317e-024	1.407e-024
*	c4	Gas	4.561e-025	1.016e-025
*	c5	Gas	1.419e-027	3.161e-028
*	n2o4	Gas	9.859e-030	2.196e-030
*	n2o5	Gas	4.367e-037	9.729e-038
*	*c solid	solid	1.449e+000	3.228e-001
*	*h2o liquid	liquid	0.000e+000	0.000e+000

Total Gas 3.633e+001 8.093e+000
 Total Cond. 1.449e+000 3.228e-001

Reference state = reactants
 $H(R) = H-62.84$, $E(R) = E-62.82$, $S(R) = S- 0.00$

	P (ATM)	V (CC/GM)	T (K)	H(R) (CAL/GM)	E(R) (CAL/GM)	S(R) (CAL/K/GM)	VGS (CC/GM)
1.)	696.6	5.6033	938.6	-1141.75	-1236.26	1.676	5.5960

Product concentrations

	Name	(mol/kg)	(mol gas/mol explosive)
*	n2	Gas	1.318e+001
*	h2o	Gas	8.023e+000
*	co2	Gas	7.781e+000
*	co	Gas	3.126e+000
*	h2	Gas	2.150e+000
*	ch4	Gas	1.729e+000
*	h3n	Gas	2.901e-001
*	c2h6	Gas	1.835e-002
*	ch2o2	Gas	1.735e-002
*	ch2o	Gas	3.414e-003
*	c2h4	Gas	2.713e-003
*	ch3oh	Gas	2.294e-003
*	chn	Gas	1.872e-003
*	chno	Gas	1.277e-003
*	ch3	Gas	2.276e-004
*	c3h8	Gas	3.856e-005
*	c3h6	Gas	2.064e-005
*	c2h2	Gas	1.924e-005
*	h	Gas	1.869e-005
*	cho	Gas	1.205e-005
*	h2n	Gas	4.527e-006
*	ho	Gas	3.073e-006
*	no	Gas	2.976e-007
*	h4n2	Gas	8.554e-008
*	h2n2	Gas	1.503e-008
*	c2n2	Gas	1.418e-008
*	cno	Gas	7.903e-009
*	c3o2	Gas	7.845e-009
*	ch2	Gas	2.639e-009
*	c2h4o	Gas	1.957e-009
*	h2o2	Gas	1.673e-009
*	hno	Gas	1.621e-009
*	cn	Gas	9.501e-010
*	n2o	Gas	5.291e-010
*	hn	Gas	3.304e-010
*	c2h	Gas	1.520e-010
*	o2	Gas	9.402e-011

*	o	Gas	5.298e-011	1.180e-011
*	c2o	Gas	1.894e-011	4.219e-012
*	n	Gas	5.752e-012	1.281e-012
*	ho2	Gas	4.443e-012	9.898e-013
*	hno2	Gas	3.294e-012	7.338e-013
*	cn2	Gas	1.849e-012	4.119e-013
*	no2h	Gas	1.647e-012	3.669e-013
*	c2n	Gas	7.691e-013	1.713e-013
*	n3	Gas	3.898e-013	8.684e-014
*	no2	Gas	2.912e-013	6.487e-014
*	ch	Gas	4.700e-014	1.047e-014
*	cnn	Gas	2.758e-016	6.143e-017
*	c	Gas	1.288e-016	2.869e-017
*	c4n2	Gas	4.458e-018	9.931e-019
*	hno3	Gas	2.100e-018	4.678e-019
*	c3	Gas	1.701e-018	3.788e-019
*	c2	Gas	8.361e-019	1.863e-019
*	no3	Gas	3.135e-022	6.983e-023
*	o3	Gas	1.438e-022	3.203e-023
*	n2o3	Gas	6.317e-024	1.407e-024
*	c4	Gas	4.561e-025	1.016e-025
*	c5	Gas	1.419e-027	3.161e-028
*	n2o4	Gas	9.859e-030	2.196e-030
*	n2o5	Gas	4.367e-037	9.729e-038
*	*c solid	solid	1.449e+000	3.228e-001
*	*h2o liquid	liquid	0.000e+000	0.000e+000
Total	Gas		3.633e+001	8.093e+000
Total	Cond.		1.449e+000	3.228e-001

Reference state = reactants
H(R) = H-62.84, E(R) = E-62.82, S(R) = S- 0.00

P (ATM)	V (CC/GM)	T (K)	H(R) (CAL/GM)	E(R) (CAL/GM)	S(R) (CAL/K/GM)	VGS (CC/GM)
1.) 237.0	11.2065	749.0	-1225.82	-1290.13	1.676	11.1993

Product concentrations

Name	(mol/kg)	(mol gas/mol explosive)
*	n2 Gas	1.318e+001 2.937e+000
*	h2o Gas	8.023e+000 1.787e+000
*	co2 Gas	7.781e+000 1.733e+000
*	co Gas	3.126e+000 6.963e-001
*	h2 Gas	2.150e+000 4.789e-001
*	ch4 Gas	1.729e+000 3.850e-001
*	h3n Gas	2.901e-001 6.462e-002
*	c2h6 Gas	1.835e-002 4.088e-003
*	ch2o2 Gas	1.735e-002 3.865e-003
*	ch2o Gas	3.414e-003 7.605e-004
*	c2h4 Gas	2.713e-003 6.044e-004
*	ch3oh Gas	2.294e-003 5.110e-004
*	chn Gas	1.872e-003 4.171e-004
*	chno Gas	1.277e-003 2.845e-004
*	ch3 Gas	2.276e-004 5.071e-005
*	c3h8 Gas	3.856e-005 8.590e-006
*	c3h6 Gas	2.064e-005 4.598e-006
*	c2h2 Gas	1.924e-005 4.286e-006
*	h Gas	1.869e-005 4.163e-006
*	cho Gas	1.205e-005 2.685e-006
*	h2n Gas	4.527e-006 1.008e-006
*	ho Gas	3.073e-006 6.846e-007
*	no Gas	2.976e-007 6.630e-008
*	h4n2 Gas	8.554e-008 1.905e-008
*	h2n2 Gas	1.503e-008 3.349e-009
*	c2n2 Gas	1.418e-008 3.160e-009
*	cno Gas	7.903e-009 1.760e-009
*	c3o2 Gas	7.845e-009 1.747e-009
*	ch2 Gas	2.639e-009 5.879e-010
*	c2h4o Gas	1.957e-009 4.359e-010

*	h2o2	Gas	1.673e-009	3.726e-010
*	hno	Gas	1.621e-009	3.612e-010
*	cn	Gas	9.501e-010	2.117e-010
*	n2o	Gas	5.291e-010	1.179e-010
*	hn	Gas	3.304e-010	7.360e-011
*	c2h	Gas	1.520e-010	3.385e-011
*	o2	Gas	9.402e-011	2.094e-011
*	o	Gas	5.298e-011	1.180e-011
*	c2o	Gas	1.894e-011	4.219e-012
*	n	Gas	5.752e-012	1.281e-012
*	ho2	Gas	4.443e-012	9.898e-013
*	hno2	Gas	3.294e-012	7.338e-013
*	cn2	Gas	1.849e-012	4.119e-013
*	no2h	Gas	1.647e-012	3.669e-013
*	c2n	Gas	7.691e-013	1.713e-013
*	n3	Gas	3.898e-013	8.684e-014
*	no2	Gas	2.912e-013	6.487e-014
*	ch	Gas	4.700e-014	1.047e-014
*	cnn	Gas	2.758e-016	6.143e-017
*	c	Gas	1.288e-016	2.869e-017
*	c4n2	Gas	4.458e-018	9.931e-019
*	hno3	Gas	2.100e-018	4.678e-019
*	c3	Gas	1.701e-018	3.788e-019
*	c2	Gas	8.361e-019	1.863e-019
*	no3	Gas	3.135e-022	6.983e-023
*	o3	Gas	1.438e-022	3.203e-023
*	n2o3	Gas	6.317e-024	1.407e-024
*	c4	Gas	4.561e-025	1.016e-025
*	c5	Gas	1.419e-027	3.161e-028
*	n2o4	Gas	9.859e-030	2.196e-030
*	n2o5	Gas	4.367e-037	9.729e-038
*	*c solid		1.449e+000	3.228e-001
*	*h2o liquid		0.000e+000	0.000e+000

Total Gas 3.633e+001 8.093e+000
 Total Cond. 1.449e+000 3.228e-001

Reference state = reactants
 $H(R) = H-62.84$, $E(R) = E-62.82$, $S(R) = S- 0.00$

P (ATM)	V (CC/GM)	T (K)	H(R) (CAL/GM)	E(R) (CAL/GM)	S(R) (CAL/K/GM)	VGS (CC/GM)
1.) 87.6	22.4131	602.1	-1280.91	-1328.42	1.676	22.4058

Product concentrations

Name	(mol/kg)	(mol gas/mol explosive)
*	n2 Gas	1.318e+001 2.937e+000
*	h2o Gas	8.023e+000 1.787e+000
*	co2 Gas	7.781e+000 1.733e+000
*	co Gas	3.126e+000 6.963e-001
*	h2 Gas	2.150e+000 4.789e-001
*	ch4 Gas	1.729e+000 3.850e-001
*	h3n Gas	2.901e-001 6.462e-002
*	c2h6 Gas	1.835e-002 4.088e-003
*	ch2o2 Gas	1.735e-002 3.865e-003
*	ch2o Gas	3.414e-003 7.605e-004
*	c2h4 Gas	2.713e-003 6.044e-004
*	ch3oh Gas	2.294e-003 5.110e-004
*	chn Gas	1.872e-003 4.171e-004
*	chno Gas	1.277e-003 2.845e-004
*	ch3 Gas	2.276e-004 5.071e-005
*	c3h8 Gas	3.856e-005 8.590e-006
*	c3h6 Gas	2.064e-005 4.598e-006
*	c2h2 Gas	1.924e-005 4.286e-006
*	h Gas	1.869e-005 4.163e-006
*	cho Gas	1.205e-005 2.685e-006
*	h2n Gas	4.527e-006 1.008e-006
*	ho Gas	3.073e-006 6.846e-007
*	no Gas	2.976e-007 6.630e-008

*	h4n2	Gas	8.554e-008	1.905e-008
*	h2n2	Gas	1.503e-008	3.349e-009
*	c2n2	Gas	1.418e-008	3.160e-009
*	cno	Gas	7.903e-009	1.760e-009
*	c3o2	Gas	7.845e-009	1.747e-009
*	ch2	Gas	2.639e-009	5.879e-010
*	c2h4o	Gas	1.957e-009	4.359e-010
*	h2o2	Gas	1.673e-009	3.726e-010
*	hno	Gas	1.621e-009	3.612e-010
*	cn	Gas	9.501e-010	2.117e-010
*	n2o	Gas	5.291e-010	1.179e-010
*	hn	Gas	3.304e-010	7.360e-011
*	c2h	Gas	1.520e-010	3.385e-011
*	o2	Gas	9.402e-011	2.094e-011
*	o	Gas	5.298e-011	1.180e-011
*	c2o	Gas	1.894e-011	4.219e-012
*	n	Gas	5.752e-012	1.281e-012
*	ho2	Gas	4.443e-012	9.898e-013
*	hno2	Gas	3.294e-012	7.338e-013
*	cn2	Gas	1.849e-012	4.119e-013
*	no2h	Gas	1.647e-012	3.669e-013
*	c2n	Gas	7.691e-013	1.713e-013
*	n3	Gas	3.898e-013	8.684e-014
*	no2	Gas	2.912e-013	6.487e-014
*	ch	Gas	4.700e-014	1.047e-014
*	cnn	Gas	2.758e-016	6.143e-017
*	c	Gas	1.288e-016	2.869e-017
*	c4n2	Gas	4.458e-018	9.931e-019
*	hno3	Gas	2.100e-018	4.678e-019
*	c3	Gas	1.701e-018	3.788e-019
*	c2	Gas	8.361e-019	1.863e-019
*	no3	Gas	3.135e-022	6.983e-023
*	o3	Gas	1.438e-022	3.203e-023
*	n2o3	Gas	6.317e-024	1.407e-024
*	c4	Gas	4.561e-025	1.016e-025
*	c5	Gas	1.419e-027	3.161e-028
*	n2o4	Gas	9.859e-030	2.196e-030
*	n2o5	Gas	4.367e-037	9.729e-038
*	*c	solid	1.449e+000	3.228e-001
*	*h2o	liquid	0.000e+000	0.000e+000

Total Gas 3.633e+001 8.093e+000
 Total Cond. 1.449e+000 3.228e-001

Reference state = reactants
 $H(R) = H-62.84$, $E(R) = E-62.82$, $S(R) = S- 0.00$

P (ATM)	V (CC/GM)	T (K)	H(R) (CAL/GM)	E(R) (CAL/GM)	S(R) (CAL/K/GM)	VGS (CC/GM)
1.) 33.6	44.8261	483.0	-1320.84	-1357.31	1.676	44.8189

Product concentrations

Name	(mol/kg)	(mol gas/mol explosive)
*	n2	Gas 1.318e+001 2.937e+000
*	h2o	Gas 8.023e+000 1.787e+000
*	co2	Gas 7.781e+000 1.733e+000
*	co	Gas 3.126e+000 6.963e-001
*	h2	Gas 2.150e+000 4.789e-001
*	ch4	Gas 1.729e+000 3.850e-001
*	h3n	Gas 2.901e-001 6.462e-002
*	c2h6	Gas 1.835e-002 4.088e-003
*	ch2o2	Gas 1.735e-002 3.865e-003
*	ch2o	Gas 3.414e-003 7.605e-004
*	c2h4	Gas 2.713e-003 6.044e-004
*	ch3oh	Gas 2.294e-003 5.110e-004
*	chn	Gas 1.872e-003 4.171e-004
*	chno	Gas 1.277e-003 2.845e-004
*	ch3	Gas 2.276e-004 5.071e-005
*	c3h8	Gas 3.856e-005 8.590e-006

*	c3h6	Gas	2.064e-005	4.598e-006
*	c2h2	Gas	1.924e-005	4.286e-006
*	h	Gas	1.869e-005	4.163e-006
*	cho	Gas	1.205e-005	2.685e-006
*	h2n	Gas	4.527e-006	1.008e-006
*	ho	Gas	3.073e-006	6.846e-007
*	no	Gas	2.976e-007	6.630e-008
*	h4n2	Gas	8.554e-008	1.905e-008
*	h2n2	Gas	1.503e-008	3.349e-009
*	c2n2	Gas	1.418e-008	3.160e-009
*	cno	Gas	7.903e-009	1.760e-009
*	c3o2	Gas	7.845e-009	1.747e-009
*	ch2	Gas	2.639e-009	5.879e-010
*	c2h4o	Gas	1.957e-009	4.359e-010
*	h2o2	Gas	1.673e-009	3.726e-010
*	hno	Gas	1.621e-009	3.612e-010
*	cn	Gas	9.501e-010	2.117e-010
*	n2o	Gas	5.291e-010	1.179e-010
*	hn	Gas	3.304e-010	7.360e-011
*	c2h	Gas	1.520e-010	3.385e-011
*	o2	Gas	9.402e-011	2.094e-011
*	o	Gas	5.298e-011	1.180e-011
*	c2o	Gas	1.894e-011	4.219e-012
*	n	Gas	5.752e-012	1.281e-012
*	ho2	Gas	4.443e-012	9.898e-013
*	hno2	Gas	3.294e-012	7.338e-013
*	cn2	Gas	1.849e-012	4.119e-013
*	no2h	Gas	1.647e-012	3.669e-013
*	c2n	Gas	7.691e-013	1.713e-013
*	n3	Gas	3.898e-013	8.684e-014
*	no2	Gas	2.912e-013	6.487e-014
*	ch	Gas	4.700e-014	1.047e-014
*	cnn	Gas	2.758e-016	6.143e-017
*	c	Gas	1.288e-016	2.869e-017
*	c4n2	Gas	4.458e-018	9.931e-019
*	hno3	Gas	2.100e-018	4.678e-019
*	c3	Gas	1.701e-018	3.788e-019
*	c2	Gas	8.361e-019	1.863e-019
*	no3	Gas	3.135e-022	6.983e-023
*	o3	Gas	1.438e-022	3.203e-023
*	n2o3	Gas	6.317e-024	1.407e-024
*	c4	Gas	4.561e-025	1.016e-025
*	c5	Gas	1.419e-027	3.161e-028
*	n2o4	Gas	9.859e-030	2.196e-030
*	n2o5	Gas	4.367e-037	9.729e-038
*	*c solid		1.449e+000	3.228e-001
*	*h2o liquid		0.000e+000	0.000e+000

Total Gas 3.633e+001 8.093e+000
 Total Cond. 1.449e+000 3.228e-001

Reference state = reactants
 $H(R) = H-62.84$, $E(R) = E-62.82$, $S(R) = S- 0.00$

P (ATM)	V (CC/GM)	T (K)	H(R) (CAL/GM)	E(R) (CAL/GM)	S(R) (CAL/K/GM)	VGS (CC/GM)
1.) 13.1	89.6523	385.1	-1351.25	-1379.69	1.676	89.6450

Product concentrations

Name	(mol/kg)	(mol gas/mol explosive)
*	n2 Gas	1.318e+001
*	h2o Gas	8.023e+000
*	co2 Gas	7.781e+000
*	co Gas	3.126e+000
*	h2 Gas	2.150e+000
*	ch4 Gas	1.729e+000
*	h3n Gas	2.901e-001
*	c2h6 Gas	1.835e-002
*	ch2o2 Gas	1.735e-002

*	ch2o	Gas	3.414e-003	7.605e-004
*	c2h4	Gas	2.713e-003	6.044e-004
*	ch3oh	Gas	2.294e-003	5.110e-004
*	chn	Gas	1.872e-003	4.171e-004
*	chno	Gas	1.277e-003	2.845e-004
*	ch3	Gas	2.276e-004	5.071e-005
*	c3h8	Gas	3.856e-005	8.590e-006
*	c3h6	Gas	2.064e-005	4.598e-006
*	c2h2	Gas	1.924e-005	4.286e-006
*	h	Gas	1.869e-005	4.163e-006
*	cho	Gas	1.205e-005	2.685e-006
*	h2n	Gas	4.527e-006	1.008e-006
*	ho	Gas	3.073e-006	6.846e-007
*	no	Gas	2.976e-007	6.630e-008
*	h4n2	Gas	8.554e-008	1.905e-008
*	h2n2	Gas	1.503e-008	3.349e-009
*	c2n2	Gas	1.418e-008	3.160e-009
*	cno	Gas	7.903e-009	1.760e-009
*	c3o2	Gas	7.845e-009	1.747e-009
*	ch2	Gas	2.639e-009	5.879e-010
*	c2h4o	Gas	1.957e-009	4.359e-010
*	h2o2	Gas	1.673e-009	3.726e-010
*	hno	Gas	1.621e-009	3.612e-010
*	cn	Gas	9.501e-010	2.117e-010
*	n2o	Gas	5.291e-010	1.179e-010
*	hn	Gas	3.304e-010	7.360e-011
*	c2h	Gas	1.520e-010	3.385e-011
*	o2	Gas	9.402e-011	2.094e-011
*	o	Gas	5.298e-011	1.180e-011
*	c2o	Gas	1.894e-011	4.219e-012
*	n	Gas	5.752e-012	1.281e-012
*	ho2	Gas	4.443e-012	9.898e-013
*	hno2	Gas	3.294e-012	7.338e-013
*	cn2	Gas	1.849e-012	4.119e-013
*	no2h	Gas	1.647e-012	3.669e-013
*	c2n	Gas	7.691e-013	1.713e-013
*	n3	Gas	3.898e-013	8.684e-014
*	no2	Gas	2.912e-013	6.487e-014
*	ch	Gas	4.700e-014	1.047e-014
*	cnn	Gas	2.758e-016	6.143e-017
*	c	Gas	1.288e-016	2.869e-017
*	c4n2	Gas	4.458e-018	9.931e-019
*	hno3	Gas	2.100e-018	4.678e-019
*	c3	Gas	1.701e-018	3.788e-019
*	c2	Gas	8.361e-019	1.863e-019
*	no3	Gas	3.135e-022	6.983e-023
*	o3	Gas	1.438e-022	3.203e-023
*	n2o3	Gas	6.317e-024	1.407e-024
*	c4	Gas	4.561e-025	1.016e-025
*	c5	Gas	1.419e-027	3.161e-028
*	n2o4	Gas	9.859e-030	2.196e-030
*	n2o5	Gas	4.367e-037	9.729e-038
*	*c solid	solid	1.449e+000	3.228e-001
*	*h2o liquid	liquid	0.000e+000	0.000e+000

Total Gas 3.633e+001 8.093e+000
 Total Cond. 1.449e+000 3.228e-001

The End of the Adiabat

Reference state = reactants
 $H(R) = H-62.84$, $E(R) = E-62.82$, $S(R) = S- 0.00$

P (ATM)	V (CC/GM)	T (K)	H(R) (CAL/GM)	E(R) (CAL/GM)	S(R) (CAL/K/GM)	VGS (CC/GM)
1.) 4.7	191.5523	298.0	-1376.90	-1398.63	1.676	191.5451

Product concentrations
 Name (mol/kg) (mol gas/mol explosive)

*	n2	Gas	1.318e+001	2.937e+000
*	h2o	Gas	8.023e+000	1.787e+000
*	co2	Gas	7.781e+000	1.733e+000
*	co	Gas	3.126e+000	6.963e-001
*	h2	Gas	2.150e+000	4.789e-001
*	ch4	Gas	1.729e+000	3.850e-001
*	h3n	Gas	2.901e-001	6.462e-002
*	c2h6	Gas	1.835e-002	4.088e-003
*	ch2o2	Gas	1.735e-002	3.865e-003
*	ch2o	Gas	3.414e-003	7.605e-004
*	c2h4	Gas	2.713e-003	6.044e-004
*	ch3oh	Gas	2.294e-003	5.110e-004
*	chn	Gas	1.872e-003	4.171e-004
*	chno	Gas	1.277e-003	2.845e-004
*	ch3	Gas	2.276e-004	5.071e-005
*	c3h8	Gas	3.856e-005	8.590e-006
*	c3h6	Gas	2.064e-005	4.598e-006
*	c2h2	Gas	1.924e-005	4.286e-006
*	h	Gas	1.869e-005	4.163e-006
*	cho	Gas	1.205e-005	2.685e-006
*	h2n	Gas	4.527e-006	1.008e-006
*	ho	Gas	3.073e-006	6.846e-007
*	no	Gas	2.976e-007	6.630e-008
*	h4n2	Gas	8.554e-008	1.905e-008
*	h2n2	Gas	1.503e-008	3.349e-009
*	c2n2	Gas	1.418e-008	3.160e-009
*	cno	Gas	7.903e-009	1.760e-009
*	c3o2	Gas	7.845e-009	1.747e-009
*	ch2	Gas	2.639e-009	5.879e-010
*	c2h4o	Gas	1.957e-009	4.359e-010
*	h2o2	Gas	1.673e-009	3.726e-010
*	hno	Gas	1.621e-009	3.612e-010
*	cn	Gas	9.501e-010	2.117e-010
*	n2o	Gas	5.291e-010	1.179e-010
*	hn	Gas	3.304e-010	7.360e-011
*	c2h	Gas	1.520e-010	3.385e-011
*	o2	Gas	9.402e-011	2.094e-011
*	o	Gas	5.298e-011	1.180e-011
*	c2o	Gas	1.894e-011	4.219e-012
*	n	Gas	5.752e-012	1.281e-012
*	ho2	Gas	4.443e-012	9.898e-013
*	hno2	Gas	3.294e-012	7.338e-013
*	cn2	Gas	1.849e-012	4.119e-013
*	no2h	Gas	1.647e-012	3.669e-013
*	c2n	Gas	7.691e-013	1.713e-013
*	n3	Gas	3.898e-013	8.684e-014
*	no2	Gas	2.912e-013	6.487e-014
*	ch	Gas	4.700e-014	1.047e-014
*	cnn	Gas	2.758e-016	6.143e-017
*	c	Gas	1.288e-016	2.869e-017
*	c4n2	Gas	4.458e-018	9.931e-019
*	hno3	Gas	2.100e-018	4.678e-019
*	c3	Gas	1.701e-018	3.788e-019
*	c2	Gas	8.361e-019	1.863e-019
*	no3	Gas	3.135e-022	6.983e-023
*	o3	Gas	1.438e-022	3.203e-023
*	n2o3	Gas	6.317e-024	1.407e-024
*	c4	Gas	4.561e-025	1.016e-025
*	c5	Gas	1.419e-027	3.161e-028
*	n2o4	Gas	9.859e-030	2.196e-030
*	n2o5	Gas	4.367e-037	9.729e-038
*	*c solid	solid	1.449e+000	3.228e-001
*	*h2o liquid	liquid	0.000e+000	0.000e+000
	Total Gas		3.633e+001	8.093e+000
	Total Cond.		1.449e+000	3.228e-001

The Products at room temperature and pressure

Reference state = reactants
 $H(R) = H-62.84$, $E(R) = E-62.82$, $S(R) = S - 0.00$

	P (ATM)	V (CC/GM)	T (K)	H(R) (CAL/GM)	E(R) (CAL/GM)	S(R) (CAL/K/GM)	VGS (CC/GM)
1.)	1.0	890.4281	298.0	-1377.09	-1398.64	1.788	890.4209

Product concentrations

	Name	(mol/kg)	(mol gas/mol explosive)
*	n2	Gas	1.318e+001 2.937e+000
*	h2o	Gas	8.023e+000 1.787e+000
*	co2	Gas	7.781e+000 1.733e+000
*	co	Gas	3.126e+000 6.963e-001
*	h2	Gas	2.150e+000 4.789e-001
*	ch4	Gas	1.729e+000 3.850e-001
*	h3n	Gas	2.901e-001 6.462e-002
*	c2h6	Gas	1.835e-002 4.088e-003
*	ch2o2	Gas	1.735e-002 3.865e-003
*	ch2o	Gas	3.414e-003 7.605e-004
*	c2h4	Gas	2.713e-003 6.044e-004
*	ch3oh	Gas	2.294e-003 5.110e-004
*	chn	Gas	1.872e-003 4.171e-004
*	chno	Gas	1.277e-003 2.845e-004
*	ch3	Gas	2.276e-004 5.071e-005
*	c3h8	Gas	3.856e-005 8.590e-006
*	c3h6	Gas	2.064e-005 4.598e-006
*	c2h2	Gas	1.924e-005 4.286e-006
*	h	Gas	1.869e-005 4.163e-006
*	cho	Gas	1.205e-005 2.685e-006
*	h2n	Gas	4.527e-006 1.008e-006
*	ho	Gas	3.073e-006 6.846e-007
*	no	Gas	2.976e-007 6.630e-008
*	h4n2	Gas	8.554e-008 1.905e-008
*	h2n2	Gas	1.503e-008 3.349e-009
*	c2n2	Gas	1.418e-008 3.160e-009
*	cno	Gas	7.903e-009 1.760e-009
*	c3o2	Gas	7.845e-009 1.747e-009
*	ch2	Gas	2.639e-009 5.879e-010
*	c2h4o	Gas	1.957e-009 4.359e-010
*	h2o2	Gas	1.673e-009 3.726e-010
*	hno	Gas	1.621e-009 3.612e-010
*	cn	Gas	9.501e-010 2.117e-010
*	n2o	Gas	5.291e-010 1.179e-010
*	hn	Gas	3.304e-010 7.360e-011
*	c2h	Gas	1.520e-010 3.385e-011
*	o2	Gas	9.402e-011 2.094e-011
*	o	Gas	5.298e-011 1.180e-011
*	c2o	Gas	1.894e-011 4.219e-012
*	n	Gas	5.752e-012 1.281e-012
*	ho2	Gas	4.443e-012 9.898e-013
*	hno2	Gas	3.294e-012 7.338e-013
*	cn2	Gas	1.849e-012 4.119e-013
*	no2h	Gas	1.647e-012 3.669e-013
*	c2n	Gas	7.691e-013 1.713e-013
*	n3	Gas	3.898e-013 8.684e-014
*	no2	Gas	2.912e-013 6.487e-014
*	ch	Gas	4.700e-014 1.047e-014
*	cnn	Gas	2.758e-016 6.143e-017
*	c	Gas	1.288e-016 2.869e-017
*	c4n2	Gas	4.458e-018 9.931e-019
*	hno3	Gas	2.100e-018 4.678e-019
*	c3	Gas	1.701e-018 3.788e-019
*	c2	Gas	8.361e-019 1.863e-019
*	no3	Gas	3.135e-022 6.983e-023
*	o3	Gas	1.438e-022 3.203e-023
*	n2o3	Gas	6.317e-024 1.407e-024
*	c4	Gas	4.561e-025 1.016e-025
*	c5	Gas	1.419e-027 3.161e-028
*	n2o4	Gas	9.859e-030 2.196e-030

```

*      n2o5   Gas    4.367e-037  9.729e-038
*      *c    solid  1.449e+000  3.228e-001
*      *h2o   liquid 0.000e+000  0.000e+000

      Total Gas   3.633e+001  8.093e+000
      Total Cond. 1.449e+000  3.228e-001
The mechanical energy of detonation = -10.444 kJ/cc
The thermal energy of detonation = -0.000 kJ/cc
The total energy of detonation = -10.444 kJ/cc

```

JWL Tail Fit results:
Initial E0 = -10.897, Final E0 = -10.835
E0(V=infty) = -10.835
C = 1.512, omega = 0.391
Final fitting error = 0.000711

V/V0	Actual E (kJ/cc)	Fit E (kJ/cc)	Actual P (GPa)	Fit P (GPa)
20.000	-9.634	-9.634	0.024	0.023
40.000	-9.919	-9.919	0.009	0.009
80.000	-10.135	-10.136	0.003	0.003
160.000	-10.302	-10.302	0.001	0.001

JWL Fit results:
E0(V=infty) = -10.835
R[1] = 4.932, R[2] = 1.074, omega = 0.391
A = 1170.029, B = 12.172, C = 1.512
Final fitting error = 0.012909

V/V0	Actual E (kJ/cc)	Fit E (kJ/cc)	Actual P (GPa)	Fit P (GPa)
0.767	3.832	3.832	32.879	34.163
1.000	-1.229	-1.382	14.153	14.108
2.200	-6.942	-6.919	1.514	1.674
4.100	-8.327	-8.466	0.361	0.361
6.500	-8.877	-8.961	0.148	0.123
10.000	-9.231	-9.260	0.071	0.062
20.000	-9.634	-9.634	0.024	0.023
40.000	-9.919	-9.919	0.009	0.009
80.000	-10.135	-10.136	0.003	0.003
160.000	-10.302	-10.302	0.001	0.001

B.2 Product library BKWC

Product library title: bkwc
Executing library command: gas eos, bkw
Executing library command: set, bkw, alpha, 0.499123809964
Executing library command: set, bkw, beta, 0.402655787895
Executing library command: set, bkw, theta, 5441.84607543
Executing library command: set, bkw, kappa, 10.8636743138
Reactant library title:# Version 2.0 by P. Clark Souers

Name	The Composition						Formula
	% wt.	% mol	% vol.	Heat of formation (cal/mol)	Standard volume (cc/mol)	Standard entropy (cal/K/mol)	
RDX	98.70	98.98	97.53	16496	122.99	0.000	222.13 C ₃ H ₆ N ₆ O ₆
Stearacid	1.30	1.02	2.47	-228967	302.30	0.000	284.47 C ₁₈ H ₃₆ O ₂

Heat of formation = 62.836 cal/gm
Standard volume = 0.560 cc/gm
Standard entropy = 0.000 cal/k/gm
Standard energy = 62.822 cal/gm

The elements and percent by mole
c 14.762

h	29.525
n	27.809
o	27.904

The average mol. wt. = 222.761 g/mol
Input>composition, rdx, 98.7, steacid, 1.3, weight
The Composition

Name	% wt.	% mol	% vol.	Heat of formation (cal/mol)	Standard volume (cc/mol)	Standard entropy (cal/K/mol)	Mol. wt.	Formula
RDX	98.70	98.98	97.53	16496	122.99	0.000	222.13	C ₃ H ₆ N ₆ O ₆
Stearacid	1.30	1.02	2.47	-228967	302.30	0.000	284.47	C ₁₈ H ₃₆ O ₂

Heat of formation = 62.836 cal/gm
Standard volume = 0.560 cc/gm
Standard entropy = 0.000 cal/k/gm
Standard energy = 62.822 cal/gm

The elements and percent by mole

c	14.762
h	29.525
n	27.809
o	27.904

The average mol. wt. = 222.761 g/mol

Input>standard run, rho, 1.784673

The hugoniot reference state:

P0 = 1.000000 ATM, V0 = 0.560327 cc/gm, E0 = 62.822270 cal/gm

Using 146576 ATM as a lower bound for the C-J pressure

Using 366441 ATM as an upper bound for the C-J pressure

The C-J point was bracketed in cjbrent

The CJ state was found in 6 iterations

The C-J condition

The shock velocity = 8.77585e+003 m/s
The particle velocity = 2.12450e+003 m/s
The speed of sound = 6.65135e+003 m/s

P0 = 1 atm, V0 = 0.56033 cc/gm, E0 = 62.82227 cal/gm

Reference state = reactants
H(R) = H-62.84, E(R) = E-62.82, S(R) = S- 0.00

P (ATM)	V (CC/GM)	T (K)	H(R) (CAL/GM)	E(R) (CAL/GM)	S(R) (CAL/K/GM)	VGS (CC/GM)
1.) 328389.9	0.4247	4147.7	3916.85	539.40	1.709	0.4044

Product concentrations

Name	(mol/kg)	(mol gas/mol explosive)
h2o Gas	1.414e+001	3.150e+000
n2 Gas	1.333e+001	2.969e+000
co2 Gas	5.699e+000	1.270e+000
co Gas	1.187e+000	2.644e-001
ch2o2 Gas	7.668e-003	1.708e-003
no Gas	7.461e-003	1.662e-003
o2 Gas	1.272e-003	2.834e-004
ch4 Gas	9.146e-004	2.037e-004
c2h4 Gas	6.513e-004	1.451e-004
h2 Gas	2.591e-004	5.771e-005
ch3oh Gas	1.831e-004	4.079e-005
h3n Gas	8.204e-005	1.828e-005
ch2o Gas	3.534e-006	7.873e-007
ch3 Gas	2.113e-009	4.707e-010
c2h6 Gas	4.239e-011	9.442e-012
no2 Gas	2.221e-013	4.948e-014
*c solid	7.257e+000	1.617e+000
Total Gas	3.437e+001	7.657e+000
Total Cond.	7.257e+000	1.617e+000

The C-J Adiabat

Reference state = reactants
 $H(R) = H-62.84$, $E(R) = E-62.82$, $S(R) = S- 0.00$

	P (ATM)	V (CC/GM)	T (K)	H(R) (CAL/GM)	E(R) (CAL/GM)	S(R) (CAL/K/GM)	VGS (CC/GM)
1.)	135993.8	0.5603	3259.6	1681.62	-163.81	1.709	0.5367

Product concentrations

Name	(mol/kg)	(mol gas/mol explosive)
h2o Gas	1.404e+001	3.128e+000
n2 Gas	1.333e+001	2.969e+000
co2 Gas	4.593e+000	1.023e+000
co Gas	3.489e+000	7.772e-001
ch4 Gas	3.032e-002	6.754e-003
ch2o2 Gas	1.568e-002	3.494e-003
h2 Gas	1.307e-002	2.912e-003
c2h4 Gas	6.803e-003	1.515e-003
h3n Gas	2.775e-003	6.182e-004
ch3oh Gas	1.339e-003	2.983e-004
no Gas	8.007e-004	1.784e-004
ch2o Gas	1.451e-004	3.231e-005
o2 Gas	1.757e-005	3.913e-006
ch3 Gas	8.612e-007	1.918e-007
c2h6 Gas	1.742e-007	3.881e-008
no2 Gas	1.481e-012	3.299e-013
*c solid	6.010e+000	1.339e+000
Total Gas	3.552e+001	7.913e+000
Total Cond.	6.010e+000	1.339e+000

Reference state = reactants
 $H(R) = H-62.84$, $E(R) = E-62.82$, $S(R) = S- 0.00$

	P (ATM)	V (CC/GM)	T (K)	H(R) (CAL/GM)	E(R) (CAL/GM)	S(R) (CAL/K/GM)	VGS (CC/GM)
1.)	14433.4	1.2327	1804.8	-465.91	-896.79	1.709	1.2217

Product concentrations

Name	(mol/kg)	(mol gas/mol explosive)
n2 Gas	1.330e+001	2.962e+000
h2o Gas	1.113e+001	2.480e+000
co Gas	5.783e+000	1.288e+000
co2 Gas	4.912e+000	1.094e+000
ch4 Gas	1.053e+000	2.347e-001
h2 Gas	7.915e-001	1.763e-001
h3n Gas	6.851e-002	1.526e-002
ch2o2 Gas	5.661e-003	1.261e-003
c2h4 Gas	4.740e-003	1.056e-003
ch2o Gas	1.235e-003	2.750e-004
ch3oh Gas	1.088e-003	2.423e-004
c2h6 Gas	5.853e-004	1.304e-004
ch3 Gas	2.187e-005	4.871e-006
no Gas	1.807e-007	4.025e-008
o2 Gas	4.061e-011	9.047e-012
no2 Gas	2.679e-015	5.967e-016
*c solid	2.386e+000	5.315e-001
Total Gas	3.705e+001	8.253e+000
Total Cond.	2.386e+000	5.315e-001

Reference state = reactants
 $H(R) = H-62.84$, $E(R) = E-62.82$, $S(R) = S- 0.00$

	P (ATM)	V (CC/GM)	T (K)	H(R) (CAL/GM)	E(R) (CAL/GM)	S(R) (CAL/K/GM)	VGS (CC/GM)
1.)	14264.1	1.2386	1800.0	-470.98	-898.84	1.709	1.2277

Product concentrations

	Name	(mol/kg)	(mol gas/mol explosive)
n2	Gas	1.330e+001	2.962e+000
h2o	Gas	1.111e+001	2.475e+000
co	Gas	5.775e+000	1.286e+000
co2	Gas	4.927e+000	1.098e+000
ch4	Gas	1.061e+000	2.363e-001
h2	Gas	7.981e-001	1.778e-001
h3n	Gas	6.877e-002	1.532e-002
ch2o2	Gas	5.604e-003	1.248e-003
c2h4	Gas	4.671e-003	1.040e-003
ch2o	Gas	1.230e-003	2.740e-004
ch3oh	Gas	1.075e-003	2.394e-004
c2h6	Gas	5.941e-004	1.323e-004
ch3	Gas	2.167e-005	4.827e-006
no	Gas	1.720e-007	3.831e-008
o2	Gas	3.780e-011	8.421e-012
no2	Gas	2.532e-015	5.640e-016
*c	solid	2.372e+000	5.283e-001
Total	Gas	3.705e+001	8.253e+000
Total	Cond.	2.372e+000	5.283e-001

Reference state = reactants

$$H(R) = H-62.84, E(R) = E-62.82, S(R) = S- 0.00$$

P (ATM)	V (CC/GM)	T (K)	H(R) (CAL/GM)	E(R) (CAL/GM)	S(R) (CAL/K/GM)	VGS (CC/GM)
1.) 3492.9	2.2973	1335.4	-882.54	-1076.86	1.709	2.2863

Product concentrations

	Name	(mol/kg)	(mol gas/mol explosive)
*	n2	Gas	1.330e+001
*	h2o	Gas	1.111e+001
*	co	Gas	5.775e+000
*	co2	Gas	4.927e+000
*	ch4	Gas	1.061e+000
*	h2	Gas	7.981e-001
*	h3n	Gas	6.877e-002
*	ch2o2	Gas	5.604e-003
*	c2h4	Gas	4.671e-003
*	ch2o	Gas	1.230e-003
*	ch3oh	Gas	1.075e-003
*	c2h6	Gas	5.941e-004
*	ch3	Gas	2.167e-005
*	no	Gas	1.720e-007
*	o2	Gas	3.780e-011
*	no2	Gas	2.532e-015
*	*c	solid	2.372e+000

Total Gas 3.705e+001 8.253e+000

Total Cond. 2.372e+000 5.283e-001

Reference state = reactants

$$H(R) = H-62.84, E(R) = E-62.82, S(R) = S- 0.00$$

P (ATM)	V (CC/GM)	T (K)	H(R) (CAL/GM)	E(R) (CAL/GM)	S(R) (CAL/K/GM)	VGS (CC/GM)
1.) 1454.8	3.6421	1115.7	-1021.13	-1149.44	1.709	3.6311

Product concentrations

	Name	(mol/kg)	(mol gas/mol explosive)
*	n2	Gas	1.330e+001
*	h2o	Gas	1.111e+001
*	co	Gas	5.775e+000
*	co2	Gas	4.927e+000
*	ch4	Gas	1.061e+000
*	h2	Gas	7.981e-001
*	h3n	Gas	6.877e-002

* ch2o2 Gas 5.604e-003 1.248e-003
 * c2h4 Gas 4.671e-003 1.040e-003
 * ch2o Gas 1.230e-003 2.740e-004
 * ch3oh Gas 1.075e-003 2.394e-004
 * c2h6 Gas 5.941e-004 1.323e-004
 * ch3 Gas 2.167e-005 4.827e-006
 * no Gas 1.720e-007 3.831e-008
 * o2 Gas 3.780e-011 8.421e-012
 * no2 Gas 2.532e-015 5.640e-016
 * *c solid 2.372e+000 5.283e-001

Total Gas 3.705e+001 8.253e+000
 Total Cond. 2.372e+000 5.283e-001

Reference state = reactants
 $H(R) = H-62.84$, $E(R) = E-62.82$, $S(R) = S- 0.00$

	P (ATM)	V (CC/GM)	T (K)	$H(R)$ (CAL/GM)	$E(R)$ (CAL/GM)	$S(R)$ (CAL/K/GM)	VGS (CC/GM)
1.)	700.9	5.6033	959.5	-1101.84	-1196.93	1.709	5.5922

Product concentrations

	Name	(mol/kg)	(mol gas/mol explosive)
*	n2 Gas	1.330e+001	2.962e+000
*	h2o Gas	1.111e+001	2.475e+000
*	co Gas	5.775e+000	1.286e+000
*	co2 Gas	4.927e+000	1.098e+000
*	ch4 Gas	1.061e+000	2.363e-001
*	h2 Gas	7.981e-001	1.778e-001
*	h3n Gas	6.877e-002	1.532e-002
*	ch2o2 Gas	5.604e-003	1.248e-003
*	c2h4 Gas	4.671e-003	1.040e-003
*	ch2o Gas	1.230e-003	2.740e-004
*	ch3oh Gas	1.075e-003	2.394e-004
*	c2h6 Gas	5.941e-004	1.323e-004
*	ch3 Gas	2.167e-005	4.827e-006
*	no Gas	1.720e-007	3.831e-008
*	o2 Gas	3.780e-011	8.421e-012
*	no2 Gas	2.532e-015	5.640e-016
*	*c solid	2.372e+000	5.283e-001

Total Gas 3.705e+001 8.253e+000
 Total Cond. 2.372e+000 5.283e-001

Reference state = reactants
 $H(R) = H-62.84$, $E(R) = E-62.82$, $S(R) = S- 0.00$

	P (ATM)	V (CC/GM)	T (K)	$H(R)$ (CAL/GM)	$E(R)$ (CAL/GM)	$S(R)$ (CAL/K/GM)	VGS (CC/GM)
1.)	241.8	11.2065	765.0	-1185.92	-1251.53	1.709	11.1955

Product concentrations

	Name	(mol/kg)	(mol gas/mol explosive)
*	n2 Gas	1.330e+001	2.962e+000
*	h2o Gas	1.111e+001	2.475e+000
*	co Gas	5.775e+000	1.286e+000
*	co2 Gas	4.927e+000	1.098e+000
*	ch4 Gas	1.061e+000	2.363e-001
*	h2 Gas	7.981e-001	1.778e-001
*	h3n Gas	6.877e-002	1.532e-002
*	ch2o2 Gas	5.604e-003	1.248e-003
*	c2h4 Gas	4.671e-003	1.040e-003
*	ch2o Gas	1.230e-003	2.740e-004
*	ch3oh Gas	1.075e-003	2.394e-004
*	c2h6 Gas	5.941e-004	1.323e-004
*	ch3 Gas	2.167e-005	4.827e-006
*	no Gas	1.720e-007	3.831e-008
*	o2 Gas	3.780e-011	8.421e-012
*	no2 Gas	2.532e-015	5.640e-016

* *c solid 2.372e+000 5.283e-001
 Total Gas 3.705e+001 8.253e+000
 Total Cond. 2.372e+000 5.283e-001

Reference state = reactants
 $H(R) = H-62.84$, $E(R) = E-62.82$, $S(R) = S- 0.00$

	P (ATM)	V (CC/GM)	T (K)	H(R) (CAL/GM)	E(R) (CAL/GM)	S(R) (CAL/K/GM)	VGS (CC/GM)
1.)	89.9	22.4131	612.9	-1241.97	-1290.73	1.709	22.4020

Product concentrations

Name	(mol/kg)	(mol gas/mol explosive)
* n2 Gas	1.330e+001	2.962e+000
* h2o Gas	1.111e+001	2.475e+000
* co Gas	5.775e+000	1.286e+000
* co2 Gas	4.927e+000	1.098e+000
* ch4 Gas	1.061e+000	2.363e-001
* h2 Gas	7.981e-001	1.778e-001
* h3n Gas	6.877e-002	1.532e-002
* ch2o2 Gas	5.604e-003	1.248e-003
* c2h4 Gas	4.671e-003	1.040e-003
* ch2o Gas	1.230e-003	2.740e-004
* ch3oh Gas	1.075e-003	2.394e-004
* c2h6 Gas	5.941e-004	1.323e-004
* ch3 Gas	2.167e-005	4.827e-006
* no Gas	1.720e-007	3.831e-008
* o2 Gas	3.780e-011	8.421e-012
* no2 Gas	2.532e-015	5.640e-016
* *c solid	2.372e+000	5.283e-001

Total Gas 3.705e+001 8.253e+000
 Total Cond. 2.372e+000 5.283e-001

Reference state = reactants
 $H(R) = H-62.84$, $E(R) = E-62.82$, $S(R) = S- 0.00$

	P (ATM)	V (CC/GM)	T (K)	H(R) (CAL/GM)	E(R) (CAL/GM)	S(R) (CAL/K/GM)	VGS (CC/GM)
1.)	34.5	44.8261	489.3	-1282.94	-1320.40	1.709	44.8151

Product concentrations

Name	(mol/kg)	(mol gas/mol explosive)
* n2 Gas	1.330e+001	2.962e+000
* h2o Gas	1.111e+001	2.475e+000
* co Gas	5.775e+000	1.286e+000
* co2 Gas	4.927e+000	1.098e+000
* ch4 Gas	1.061e+000	2.363e-001
* h2 Gas	7.981e-001	1.778e-001
* h3n Gas	6.877e-002	1.532e-002
* ch2o2 Gas	5.604e-003	1.248e-003
* c2h4 Gas	4.671e-003	1.040e-003
* ch2o Gas	1.230e-003	2.740e-004
* ch3oh Gas	1.075e-003	2.394e-004
* c2h6 Gas	5.941e-004	1.323e-004
* ch3 Gas	2.167e-005	4.827e-006
* no Gas	1.720e-007	3.831e-008
* o2 Gas	3.780e-011	8.421e-012
* no2 Gas	2.532e-015	5.640e-016
* *c solid	2.372e+000	5.283e-001

Total Gas 3.705e+001 8.253e+000
 Total Cond. 2.372e+000 5.283e-001

Reference state = reactants
 $H(R) = H-62.84$, $E(R) = E-62.82$, $S(R) = S- 0.00$

P	V	T	H(R)	E(R)	S(R)	VGS
---	---	---	------	------	------	-----

	(ATM)	(CC/GM)	(K)	(CAL/GM)	(CAL/GM)	(CAL/K/GM)	(CC/GM)
1.)	13.4	89.6523	388.5	-1314.21	-1343.37	1.709	89.6412

Product concentrations

	Name	(mol/kg)	(mol gas/mol explosive)
*	n2	Gas	1.330e+001 2.962e+000
*	h2o	Gas	1.111e+001 2.475e+000
*	co	Gas	5.775e+000 1.286e+000
*	co2	Gas	4.927e+000 1.098e+000
*	ch4	Gas	1.061e+000 2.363e-001
*	h2	Gas	7.981e-001 1.778e-001
*	h3n	Gas	6.877e-002 1.532e-002
*	ch2o2	Gas	5.604e-003 1.248e-003
*	c2h4	Gas	4.671e-003 1.040e-003
*	ch2o	Gas	1.230e-003 2.740e-004
*	ch3oh	Gas	1.075e-003 2.394e-004
*	c2h6	Gas	5.941e-004 1.323e-004
*	ch3	Gas	2.167e-005 4.827e-006
*	no	Gas	1.720e-007 3.831e-008
*	o2	Gas	3.780e-011 8.421e-012
*	no2	Gas	2.532e-015 5.640e-016
*	*c	solid	2.372e+000 5.283e-001
Total	Gas	3.705e+001	8.253e+000
Total	Cond.	2.372e+000	5.283e-001

The End of the Adiabat

Reference state = reactants

H(R) = H-62.84, E(R) = E-62.82, S(R) = S- 0.00

	P (ATM)	V (CC/GM)	T (K)	H(R) (CAL/GM)	E(R) (CAL/GM)	S(R) (CAL/K/GM)	VGS (CC/GM)
1.)	4.7	194.5069	298.0	-1340.99	-1363.12	1.709	194.4959

Product concentrations

	Name	(mol/kg)	(mol gas/mol explosive)
*	n2	Gas	1.330e+001 2.962e+000
*	h2o	Gas	1.111e+001 2.475e+000
*	co	Gas	5.775e+000 1.286e+000
*	co2	Gas	4.927e+000 1.098e+000
*	ch4	Gas	1.061e+000 2.363e-001
*	h2	Gas	7.981e-001 1.778e-001
*	h3n	Gas	6.877e-002 1.532e-002
*	ch2o2	Gas	5.604e-003 1.248e-003
*	c2h4	Gas	4.671e-003 1.040e-003
*	ch2o	Gas	1.230e-003 2.740e-004
*	ch3oh	Gas	1.075e-003 2.394e-004
*	c2h6	Gas	5.941e-004 1.323e-004
*	ch3	Gas	2.167e-005 4.827e-006
*	no	Gas	1.720e-007 3.831e-008
*	o2	Gas	3.780e-011 8.421e-012
*	no2	Gas	2.532e-015 5.640e-016
*	*c	solid	2.372e+000 5.283e-001
Total	Gas	3.705e+001	8.253e+000
Total	Cond.	2.372e+000	5.283e-001

The Products at room temperature and pressure

Reference state = reactants

H(R) = H-62.84, E(R) = E-62.82, S(R) = S- 0.00

	P (ATM)	V (CC/GM)	T (K)	H(R) (CAL/GM)	E(R) (CAL/GM)	S(R) (CAL/K/GM)	VGS (CC/GM)
1.)	1.0	907.7454	298.0	-1341.16	-1363.13	1.823	907.7344

Product concentrations

	Name	(mol/kg)	(mol gas/mol explosive)
*	n2	Gas	1.330e+001 2.962e+000
*	h2o	Gas	1.111e+001 2.475e+000
*	co	Gas	5.775e+000 1.286e+000
*	co2	Gas	4.927e+000 1.098e+000
*	ch4	Gas	1.061e+000 2.363e-001
*	h2	Gas	7.981e-001 1.778e-001
*	h3n	Gas	6.877e-002 1.532e-002
*	ch2o2	Gas	5.604e-003 1.248e-003
*	c2h4	Gas	4.671e-003 1.040e-003
*	ch2o	Gas	1.230e-003 2.740e-004
*	ch3oh	Gas	1.075e-003 2.394e-004
*	c2h6	Gas	5.941e-004 1.323e-004
*	ch3	Gas	2.167e-005 4.827e-006
*	no	Gas	1.720e-007 3.831e-008
*	o2	Gas	3.780e-011 8.421e-012
*	no2	Gas	2.532e-015 5.640e-016
*	*c	solid	2.372e+000 5.283e-001

Total Gas 3.705e+001 8.253e+000
 Total Cond. 2.372e+000 5.283e-001

The mechanical energy of detonation = -10.179 kJ/cc
 The thermal energy of detonation = -0.000 kJ/cc
 The total energy of detonation = -10.179 kJ/cc

JWL Tail Fit results:

Initial E0 = -10.638, Final E0 = -10.583
 E0(V=infty) = -10.583
 C = 1.536, omega = 0.388
 Final fitting error = 0.000603

V/V0	Actual E (kJ/cc)	Fit E (kJ/cc)	Actual P (GPa)	Fit P (GPa)
20.000	-9.345	-9.345	0.025	0.024
40.000	-9.638	-9.637	0.009	0.009
80.000	-9.860	-9.860	0.003	0.004
160.000	-10.031	-10.031	0.001	0.001

JWL Fit results:

E0(V=infty) = -10.583
 R[1] = 4.766, R[2] = 1.068, omega = 0.388
 A = 995.590, B = 10.948, C = 1.536
 Final fitting error = 0.009871

V/V0	Actual E (kJ/cc)	Fit E (kJ/cc)	Actual P (GPa)	Fit P (GPa)
0.758	4.028	4.028	33.274	34.012
1.000	-1.223	-1.323	13.780	13.780
2.200	-6.696	-6.685	1.462	1.586
4.100	-8.041	-8.165	0.354	0.354
6.500	-8.583	-8.659	0.147	0.125
10.000	-8.938	-8.963	0.071	0.063
20.000	-9.345	-9.345	0.025	0.024
40.000	-9.638	-9.637	0.009	0.009
80.000	-9.860	-9.860	0.003	0.004
160.000	-10.031	-10.031	0.001	0.001

Appendix C Summary printouts

C.1 Density TMD (1.7847 g/cm³)

C.1.1 Product library BKWS

Product library title: bkws library
 Reactant library title: # Version 2.0 by P. Clark Souers

Name	% wt.	% mol	% vol	The composition:		TMD (g/cc)
				Heat of formation (cal/mol)	Mol. wt.	
Stearacid	1.30	1.02	2.47	-228967	284.47	0.94 <chem>C18H36O2</chem>
RDX	98.70	98.98	97.53	16496	222.13	1.81 <chem>C3H6N6O6</chem>

Density = 1.7847 g/cc Mixture TMD = 1.7847 g/cc % TMD = 100.0000

The C-J condition:

The pressure	=	32.88 GPa
The volume	=	0.430 cc/g
The density	=	2.327 g/cc
The energy	=	3.83 kJ/cc explosive
The temperature	=	4085 K
The shock velocity	=	8.891 mm/us
The particle velocity	=	2.072 mm/us
The speed of sound	=	6.818 mm/us
Gamma	=	3.290

Cylinder runs: V/V ₀ (rel.)	Energy (kJ/cc)	% of standards				
		TATB 1.83g/cc	PETN 1.76g/cc	HMX 1.89g/cc	CL-20 2.04g/cc	TRITON 1.70g/cc
1.00	-1.23					
2.20	-6.94	143	109	93	77	159
4.10	-8.33	143	108	94	79	151
6.50	-8.88	142	107	94	80	145
10.00	-9.23	142	106	94	80	141
20.00	-9.63	140	105	95	81	134
40.00	-9.92	139	104	95	82	128
80.00	-10.14	138	104	95	82	123
160.00	-10.30					

Freezing occurred at T = 1800.0 K and relative V = 2.196
 The mechanical energy of detonation = -10.444 kJ/cc
 The thermal energy of detonation = -0.000 kJ/cc
 The total energy of detonation = -10.444 kJ/cc

JWL Fit results:

E0 = -10.835 kJ/cc
 A = 1170.03 GPa, B = 12.17 GPa , C = 1.51 GPa
 R[1] = 4.93, R[2] = 1.07, omega = 0.39

RMS fitting error = 1.29 %

C.1.2 Product library BKWC

Product library title: bkwc
 Reactant library title: # Version 2.0 by P. Clark Souers

The composition:

Name	% wt.	% mol	% vol	The composition:		TMD (g/cc)
				Heat of formation (cal/mol)	Mol. wt.	
RDX	98.70	98.98	97.53	16496	222.13	1.81 <chem>C3H6N6O6</chem>
Stearacid	1.30	1.02	2.47	-228967	284.47	0.94 <chem>C18H36O2</chem>

Density = 1.7847 g/cc Mixture TMD = 1.7847 g/cc % TMD = 100.0000

The C-J condition:

The pressure	=	33.27 GPa
The volume	=	0.425 cc/g
The density	=	2.355 g/cc
The energy	=	4.03 kJ/cc explosive
The temperature	=	4148 K
The shock velocity	=	8.776 mm/us
The particle velocity	=	2.125 mm/us
The speed of sound	=	6.651 mm/us
Gamma	=	3.131

Cylinder runs:

V/V ₀ (rel.)	Energy (kJ/cc)	% of standards				
		TATB 1.83g/cc	PETN 1.76g/cc	HMX 1.89g/cc	CL-20 2.04g/cc	TRITON 1.70g/cc
1.00	-1.22					
2.20	-6.70	138	105	90	74	154
4.10	-8.04	138	104	91	76	146
6.50	-8.58	138	103	91	77	140
10.00	-8.94	137	103	91	78	136
20.00	-9.35	136	102	92	79	130
40.00	-9.64	135	101	92	79	125
80.00	-9.86	134	101	92	80	120
160.00	-10.03					

Freezing occurred at T = 1800.0 K and relative V = 2.210
The mechanical energy of detonation = -10.179 kJ/cc
The thermal energy of detonation = -0.000 kJ/cc
The total energy of detonation = -10.179 kJ/cc

JWL Fit results:

E ₀	=	-10.583 kJ/cc						
A	=	995.59 GPa, B	=	10.95 GPa	,	C	=	1.54 GPa
R[1]	=	4.77,	R[2]	=	1.07,	omega	=	0.39
RMS fitting error	=	0.99 %						

C.2 Density 1.702 g/cm³

C.2.1 Product library BKWS

Product library title: bkws library
Reactant library title: # Version 2.0 by P. Clark Souers

The composition:

Name	% wt.	% mol	% vol	Heat of formation (cal/mol)	Mol. wt.	TMD (g/cc)
rdx	98.70	98.98	97.53	16496	222.13	1.81 c3h6n6o6
steacid	1.30	1.02	2.47	-228967	284.47	0.94 c18h36o2

Density = 1.7020 g/cc Mixture TMD = 1.7847 g/cc % TMD = 95.3676

The C-J condition:

The pressure	=	29.57 GPa
The volume	=	0.448 cc/g
The density	=	2.233 g/cc
The energy	=	3.52 kJ/cc explosive
The temperature	=	4140 K
The shock velocity	=	8.549 mm/us
The particle velocity	=	2.032 mm/us
The speed of sound	=	6.517 mm/us
Gamma	=	3.206

Cylinder runs: % of standards

V/V ₀ (rel.)	Energy (kJ/cc)	TATB 1.83g/cc	PETN 1.76g/cc	HMX 1.89g/cc	CL-20 2.04g/cc	TRITON 1.70g/cc

1.00	-1.13					
2.20	-6.41	132	101	86	71	147
4.10	-7.74	133	100	87	73	140
6.50	-8.27	133	100	88	74	135
10.00	-8.62	132	99	88	75	131
20.00	-9.02	131	98	88	76	126
40.00	-9.30	130	98	89	77	120
80.00	-9.51	129	97	89	77	115
160.00	-9.68					

Freezing occurred at T = 1800.0 K and relative V = 2.279
The mechanical energy of detonation = -9.825 kJ/cc
The thermal energy of detonation = -0.000 kJ/cc
The total energy of detonation = -9.825 kJ/cc

JWL Fit results:

E0 = -10.132 kJ/cc
A = 1007.40 GPa, B = 11.73 GPa, C = 1.76 GPa
R[1] = 4.96, R[2] = 1.12, omega = 0.43
RMS fitting error = 1.02 %

C.2.2 Product library BKWC

Product library title: bkwc

Reactant library title: # Version 2.0 by P. Clark Souers

The composition:

Name	% wt.	% mol	% vol	Heat of formation (cal/mol)	Mol. wt.	TMD (g/cc)
rdx	98.70	98.98	97.53	16496	222.13	1.81 c3h6n6o6
steacid	1.30	1.02	2.47	-228967	284.47	0.94 c18h36o2

Density = 1.7020 g/cc Mixture TMD = 1.7847 g/cc % TMD = 95.3676

The C-J condition:

The pressure = 29.74 GPa
The volume = 0.444 cc/g
The density = 2.250 g/cc
The energy = 3.62 kJ/cc explosive
The temperature = 4191 K
The shock velocity = 8.471 mm/us
The particle velocity = 2.063 mm/us
The speed of sound = 6.408 mm/us
Gamma = 3.107

Cylinder runs: % of standards

V/V0 (rel.)	Energy (kJ/cc)	TATB 1.83g/cc	PETN 1.76g/cc	HMX 1.89g/cc	CL-20 2.04g/cc	TRITON 1.70g/cc
1.00	-1.11					
2.20	-6.16	127	97	83	68	141
4.10	-7.46	128	97	84	71	135
6.50	-7.99	128	96	85	72	131
10.00	-8.33	128	96	85	73	127
20.00	-8.73	127	95	86	74	122
40.00	-9.02	126	95	86	74	117
80.00	-9.24	125	95	86	75	112
160.00	-9.41					

Freezing occurred at T = 1800.0 K and relative V = 2.292
The mechanical energy of detonation = -9.554 kJ/cc
The thermal energy of detonation = -0.000 kJ/cc
The total energy of detonation = -9.554 kJ/cc

JWL Fit results:

E0 = -9.879 kJ/cc
A = 884.93 GPa, B = 10.23 GPa, C = 1.75 GPa
R[1] = 4.80, R[2] = 1.11, omega = 0.43
RMS fitting error = 0.77 %

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